



Integrated Hybrid Life Cycle Optimization for Multi-Scale Sustainability Analytics of Energy Systems

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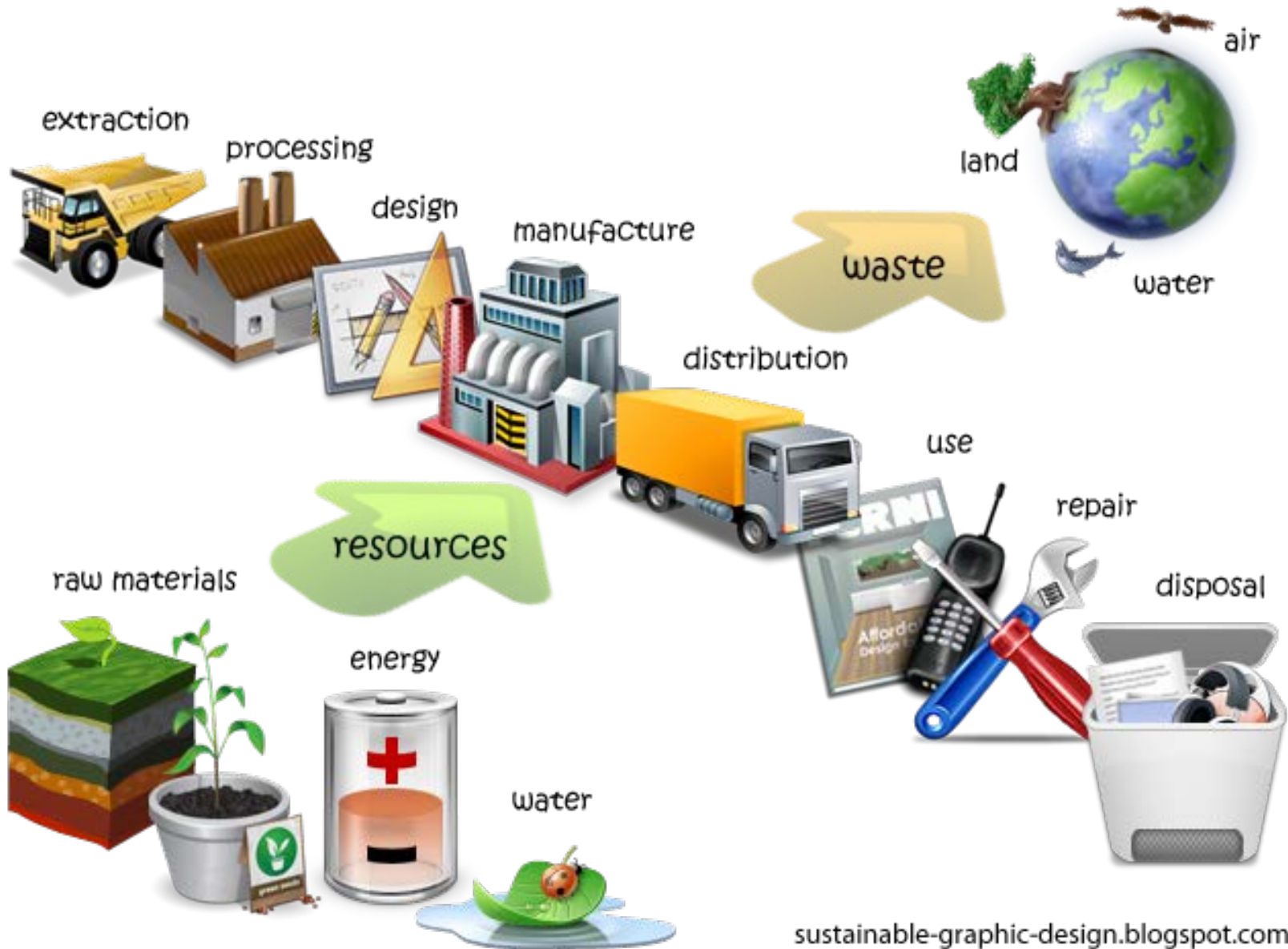
3rd SEE SDEWES, Novi Sad, July 2018



Environmental Sustainability Issues

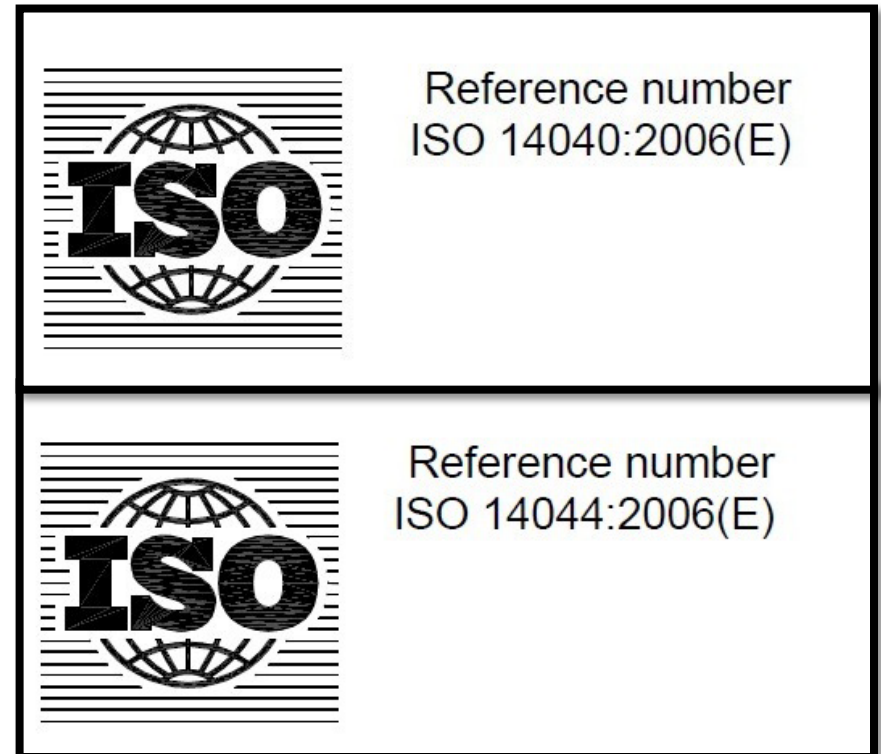
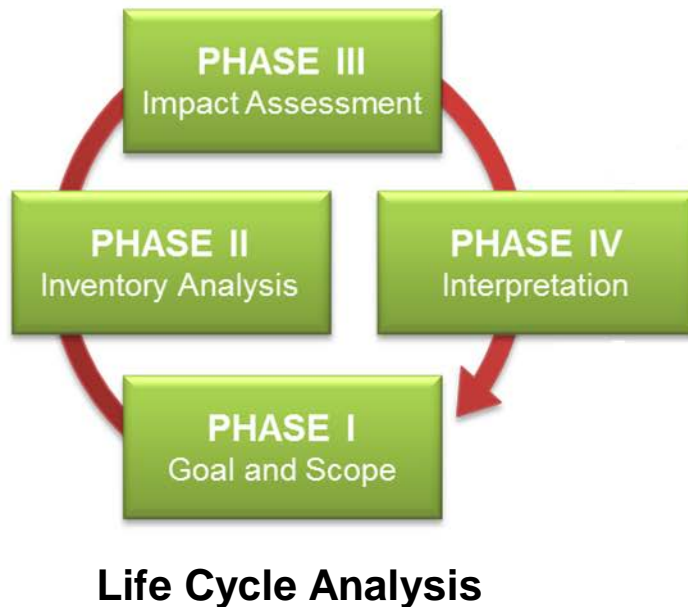


Life Cycle Analysis (LCA) – “Cradle to Grave”



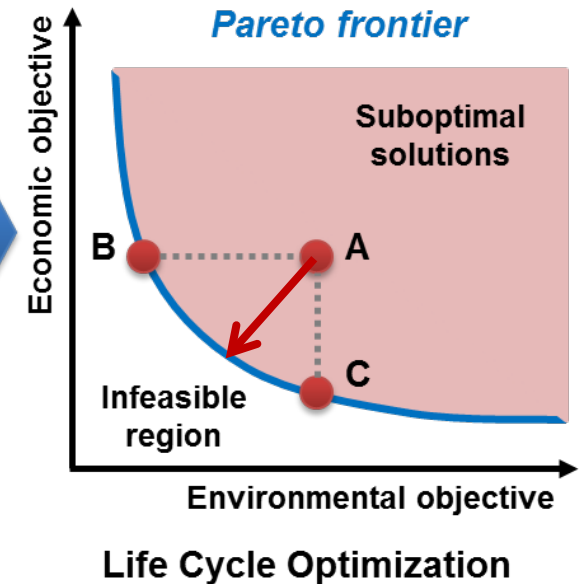
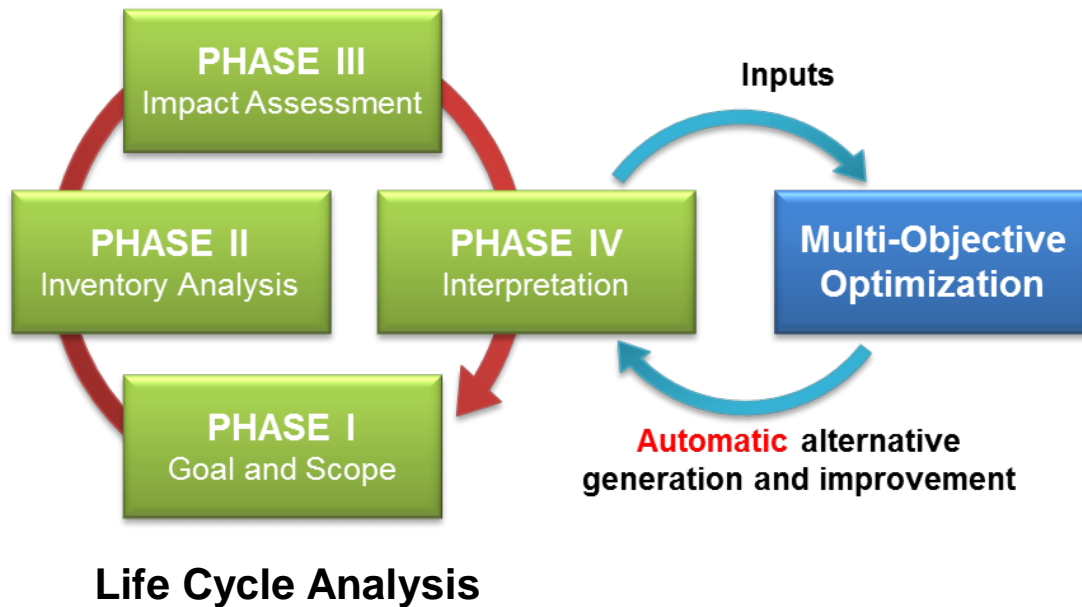
Life Cycle Analysis (LCA)

- Quantifying environmental impacts of **complex systems**
- Modeling the entire product/process **life cycle**
- Holistic view of the system



Life Cycle Optimization (LCO)

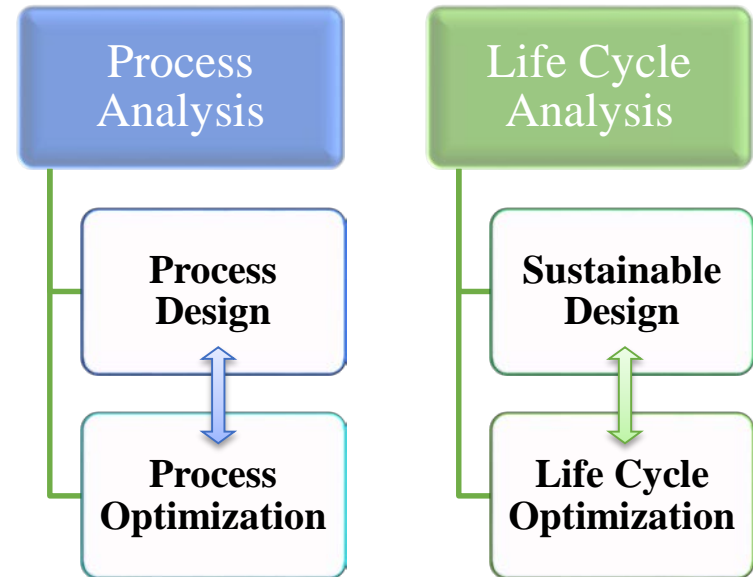
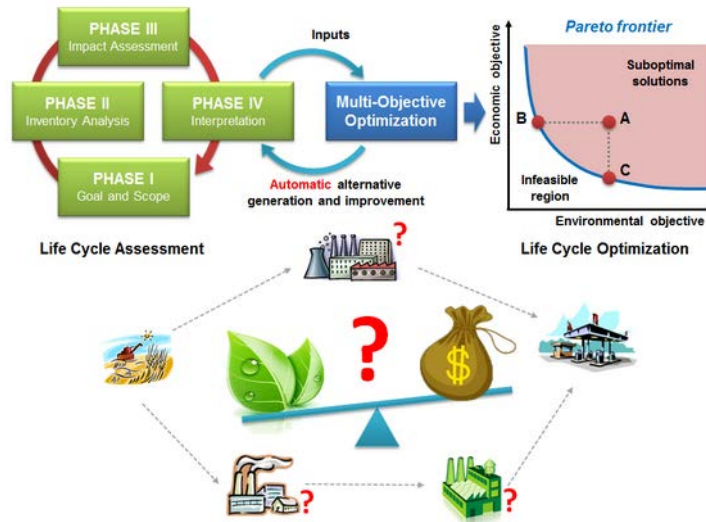
Integrating life cycle analysis approach with multi-objective optimization techniques



Life Cycle Optimization: Theory and Methods

- **Life Cycle Optimization**

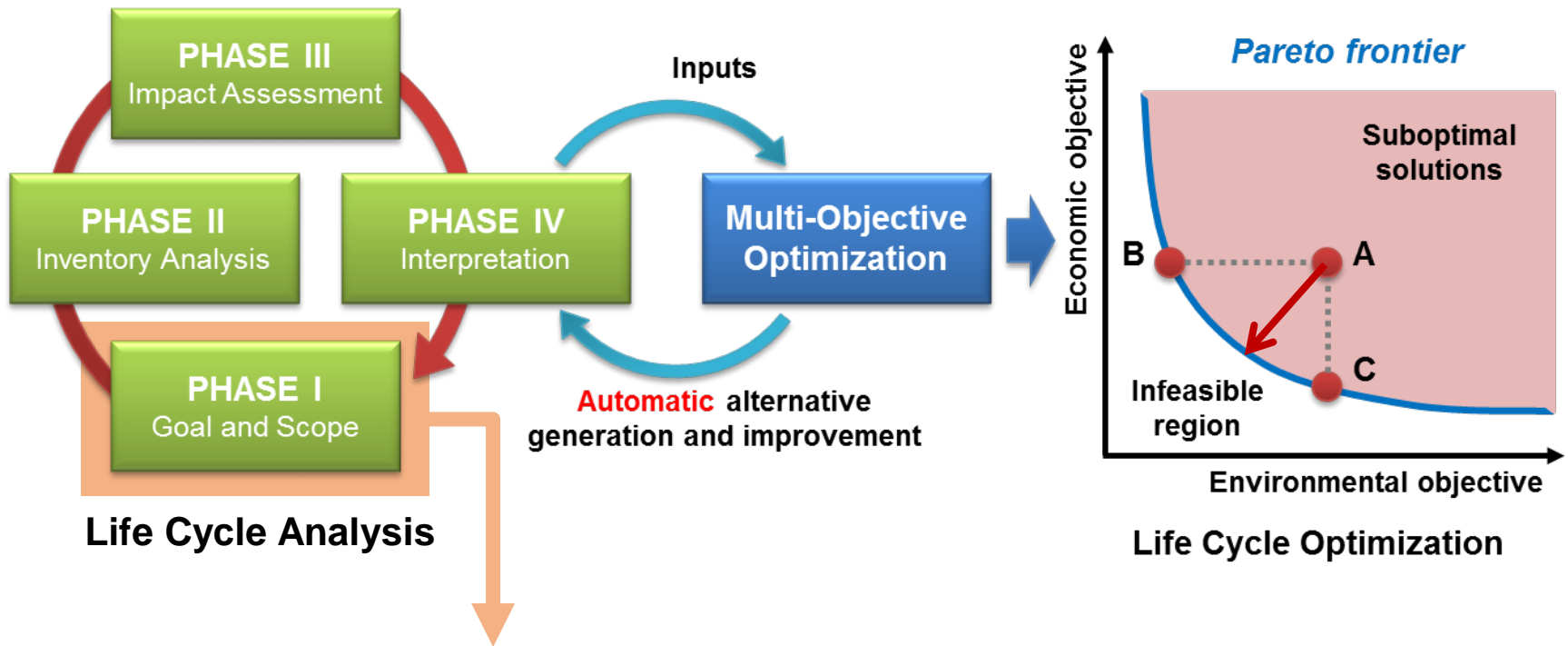
- Life Cycle Analysis + Techno-economic Analysis + Design Optimization



- **Research Challenges**

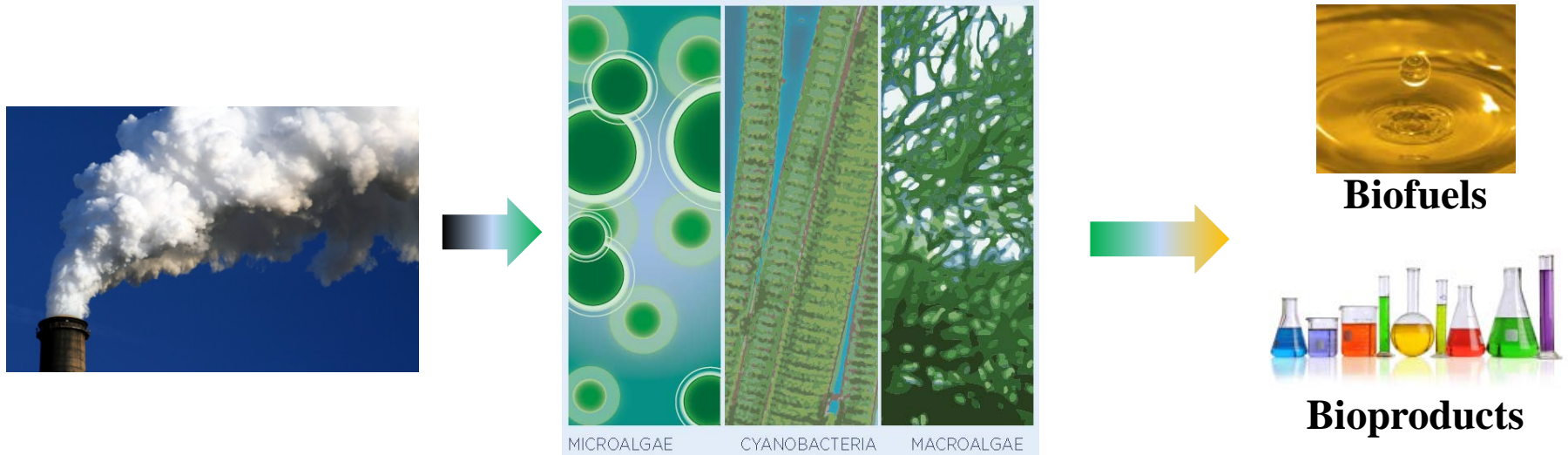
- How to **seamlessly** integrate LCA into process systems optimization?
- How to define the “optimal” **systems boundary** and **functional unit**?
- How to incorporate state-of-the-art **inventory analysis** methods in LCO?
- How to deal with **uncertainty** and solve **large-scale** LCO problems?

Process-based Life Cycle Optimization (LCO)



- **Systems boundary** must be defined in Phase I of LCA
- **Functional unit** serves as the basis for calculation and comparison

Motivation



- **Algae**

- Microalgae, cyanobacteria, & macroalgae
- Non-food; high yield; rich in oil

- **Algae-based biorefinery**

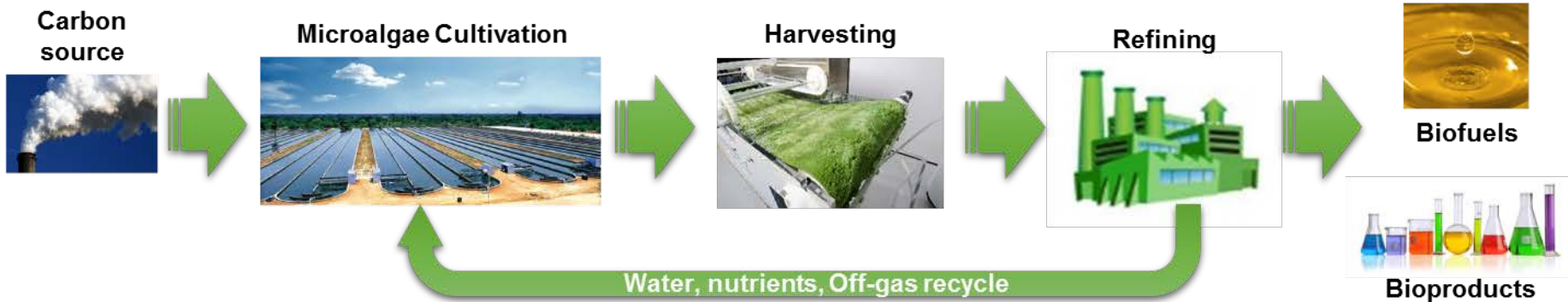
- Consume and utilize CO₂; recycle nutrients & water
- Produce fuels and value-added products

- **Process economics? Environmental sustainability?**

Chlorella Vulgaris



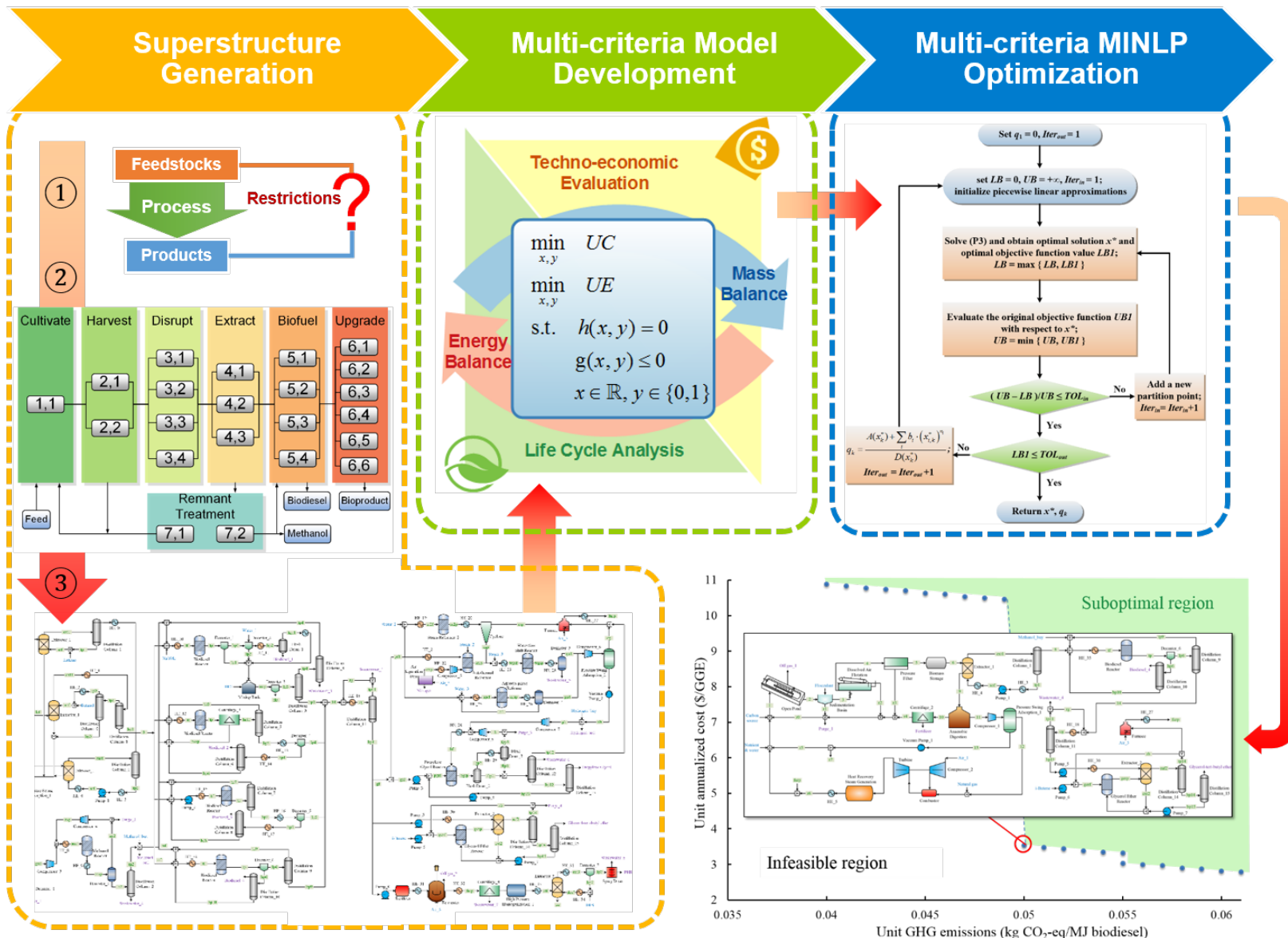
Algal Biorefinery Process Design and Optimization



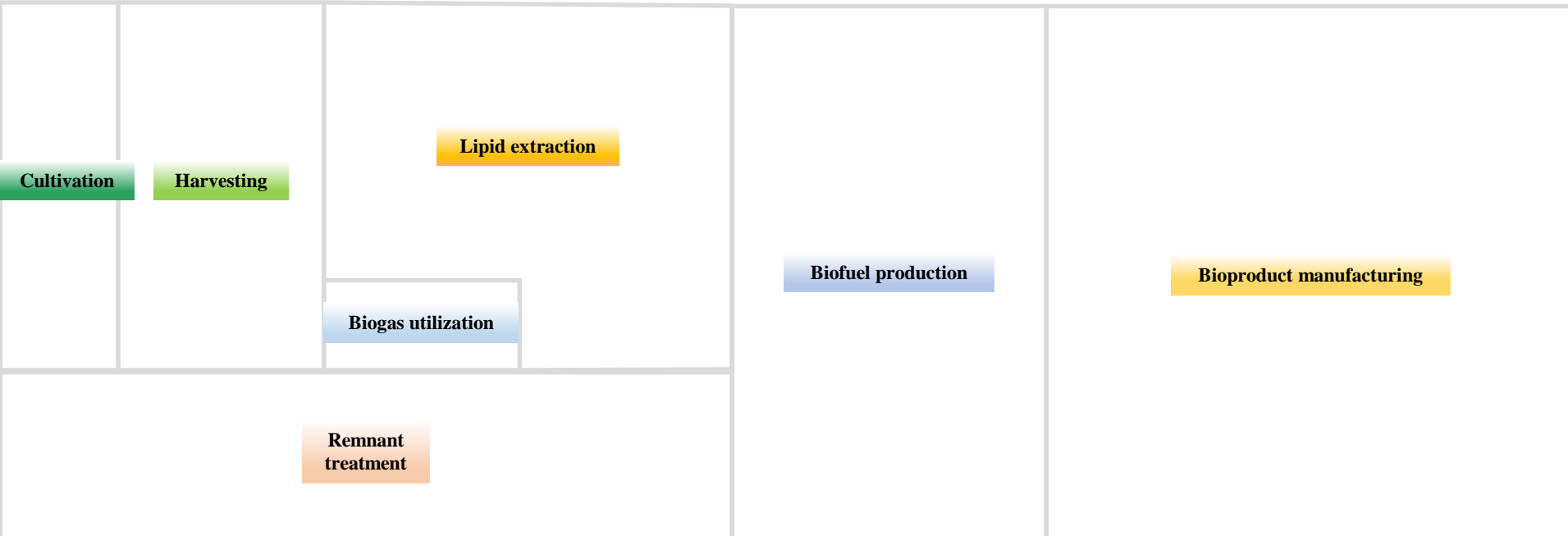
- **Optimal design and synthesis of algal biorefinery**
 - Selection of technology, pathway, and processing methods
 - Determination of product portfolio under the given feed
 - Recycling nutrients, water and carbon dioxide
 - Mass balance, capacity, and equipment sizing
 - Energy and utility consumption
 - Process economics ? → **Techno-economic analysis**
 - Environmental sustainability ? → **Life cycle analysis**
 - Cost-effective & sustainable design



LCO for Sustainable Design of Energy Systems



Superstructure of Algae Process

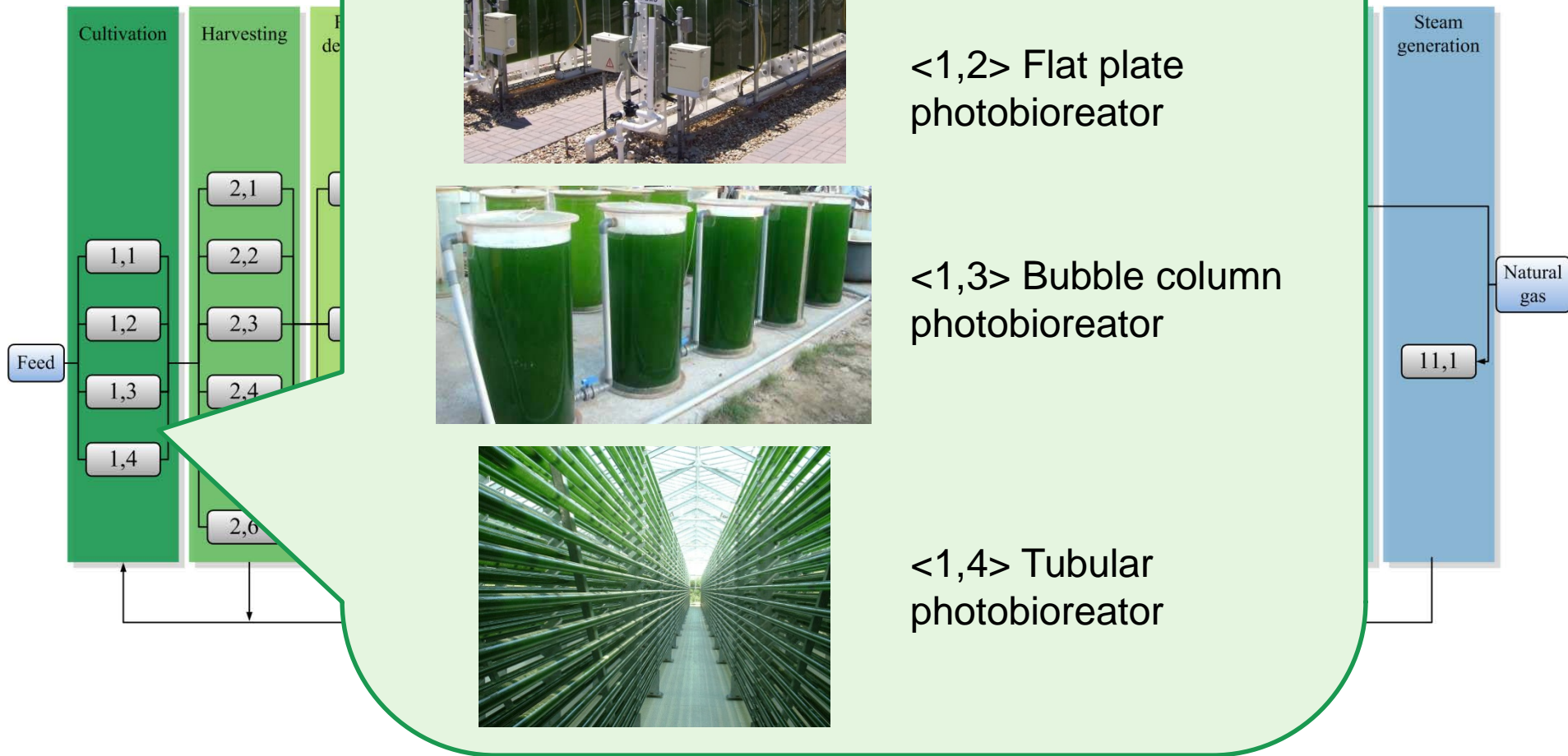


Biodiesel
Diesel



Hydrogen
Propylene glycol
Glycerol-tert-butyl ether
Poly-3-hydroxybutyrate

Superstructure of Algae Process



7,800+ processing pathways

Optimization Model: Constraints for ONE Unit

Mass and material balance

Process network design specifications
Technology and pathway selection
Equipment sizing and capacity

**Techno-economic
analysis**

Energy balance

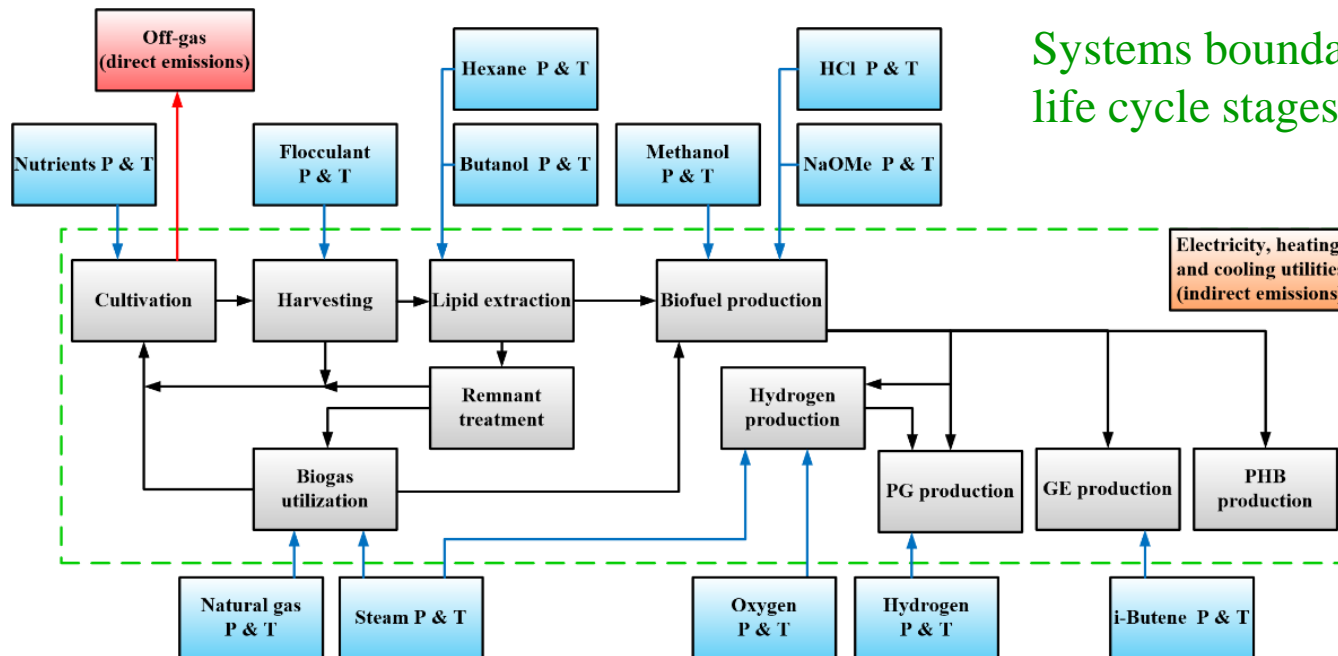
Utility consumption

**Life cycle environmental
impact analysis**

Optimization Model: Objectives

- **Objectives:**

- Minimize: **Unit cost of fuel product (techno-economic analysis)**
 - CAPEX + OPEX
 - Credit from selling by-products (glycerol, fertilizer, biogas, ...)
- Minimize: **Unit life cycle GHG emission (life cycle analysis)**
 - **Direct emissions:** Cultivation, remnant treatment, & utility generation
 - **Indirect emissions:** External utility, e.g. electricity and steam, ...



Systems boundary and life cycle stages of LCA

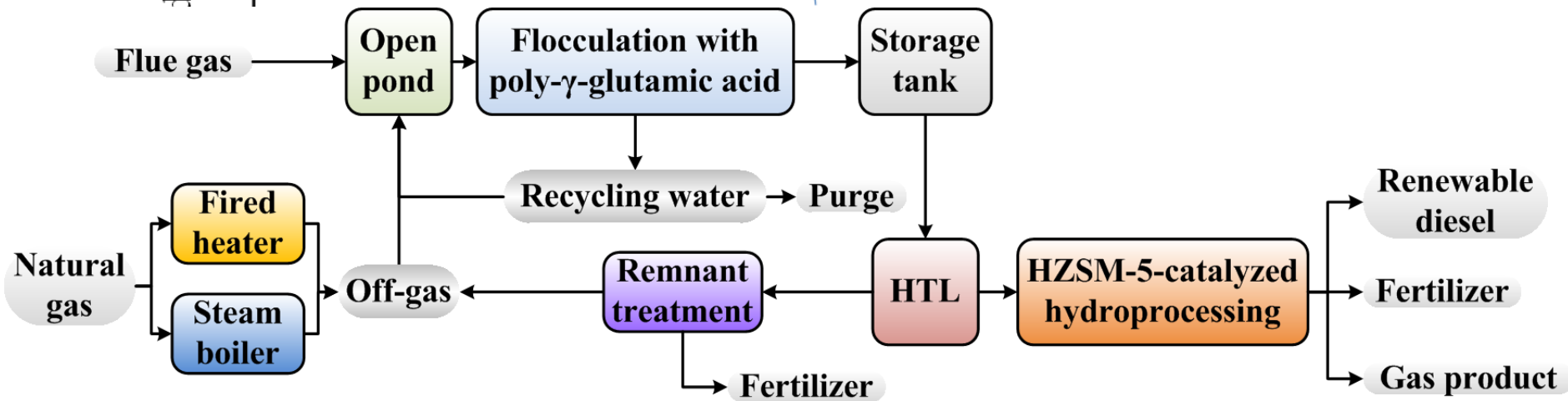
Pareto Optimal Curve

12
10
8
1 cost (\$/GGE)

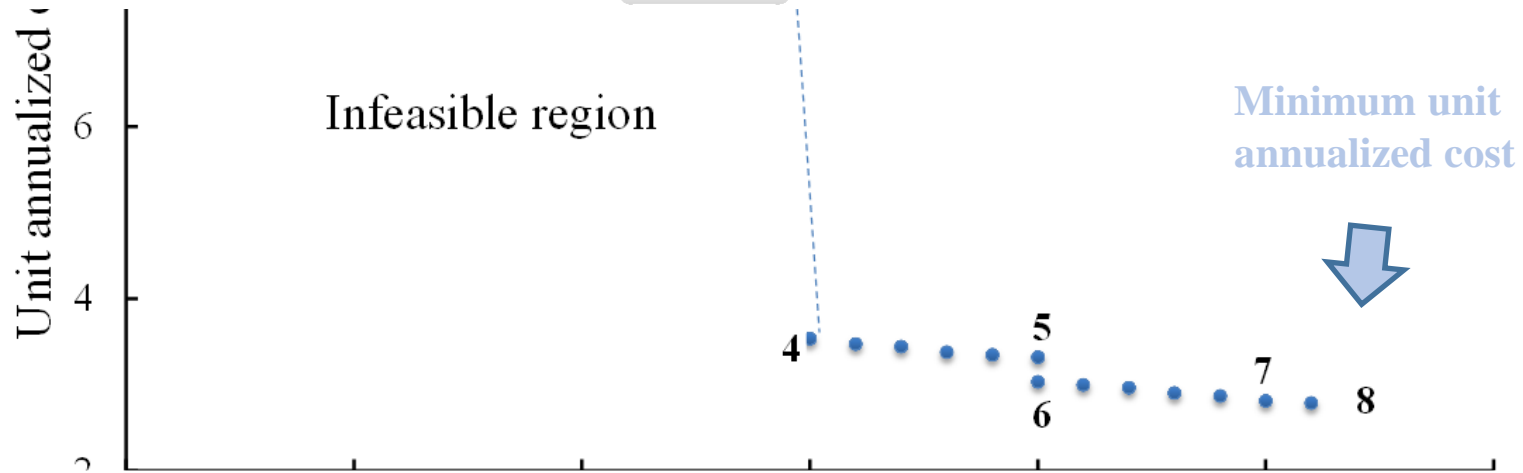
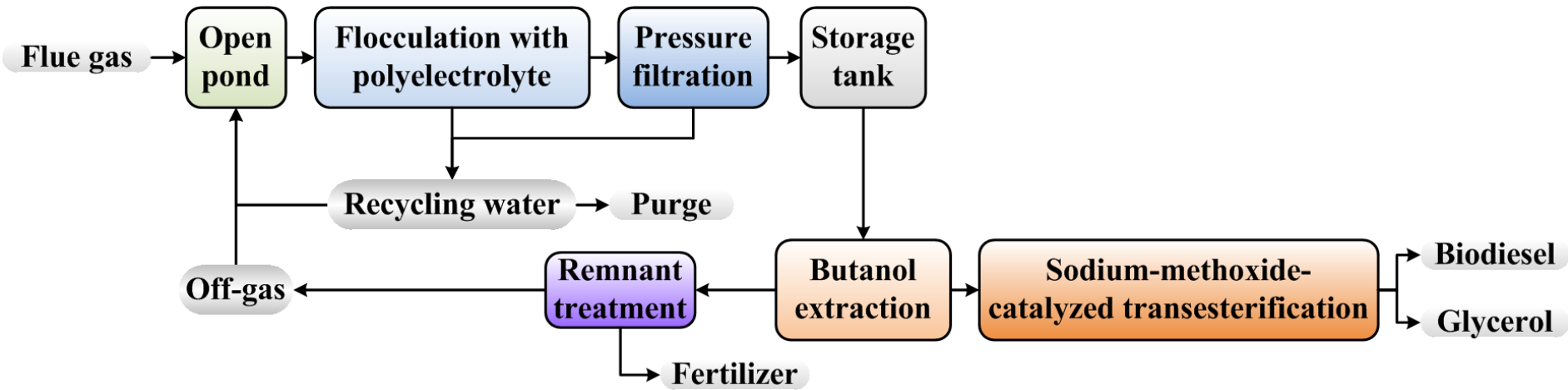
1 2 3

Minimum unit GWP

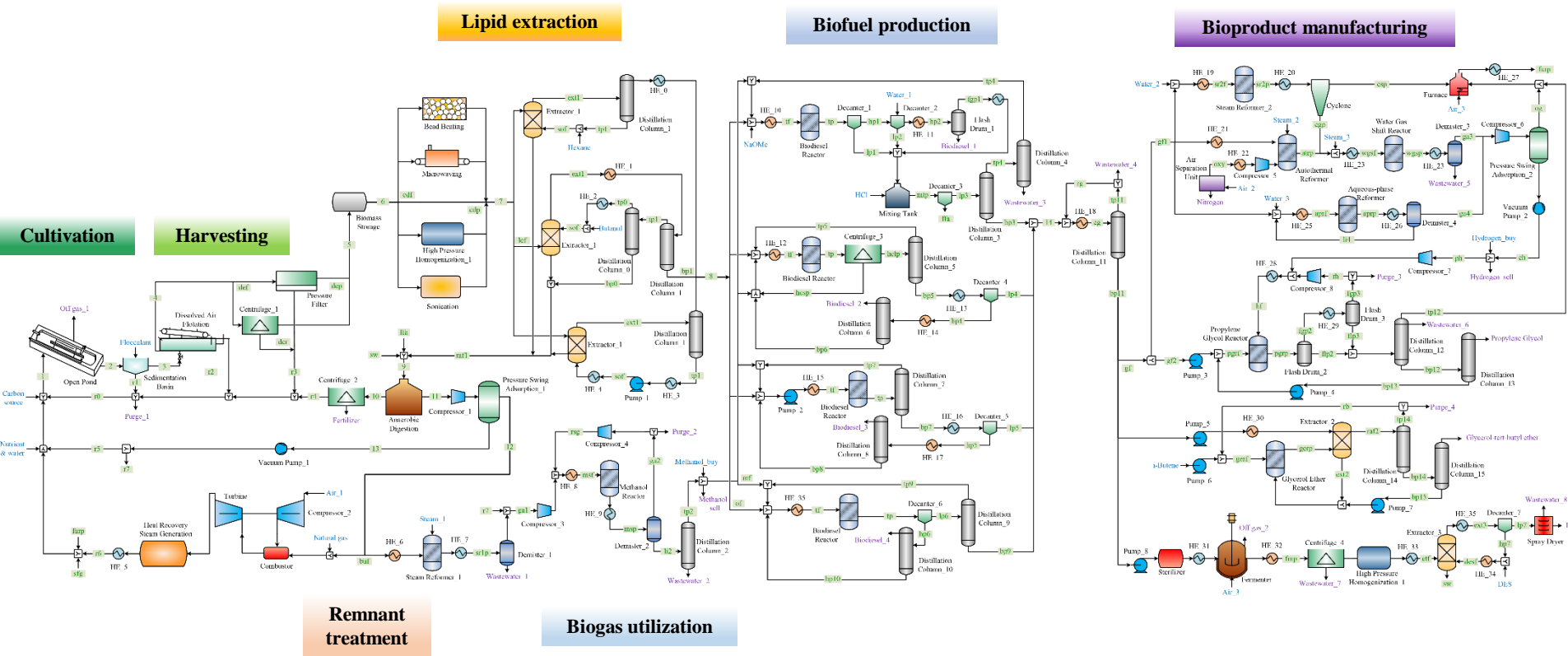
Suboptimal region



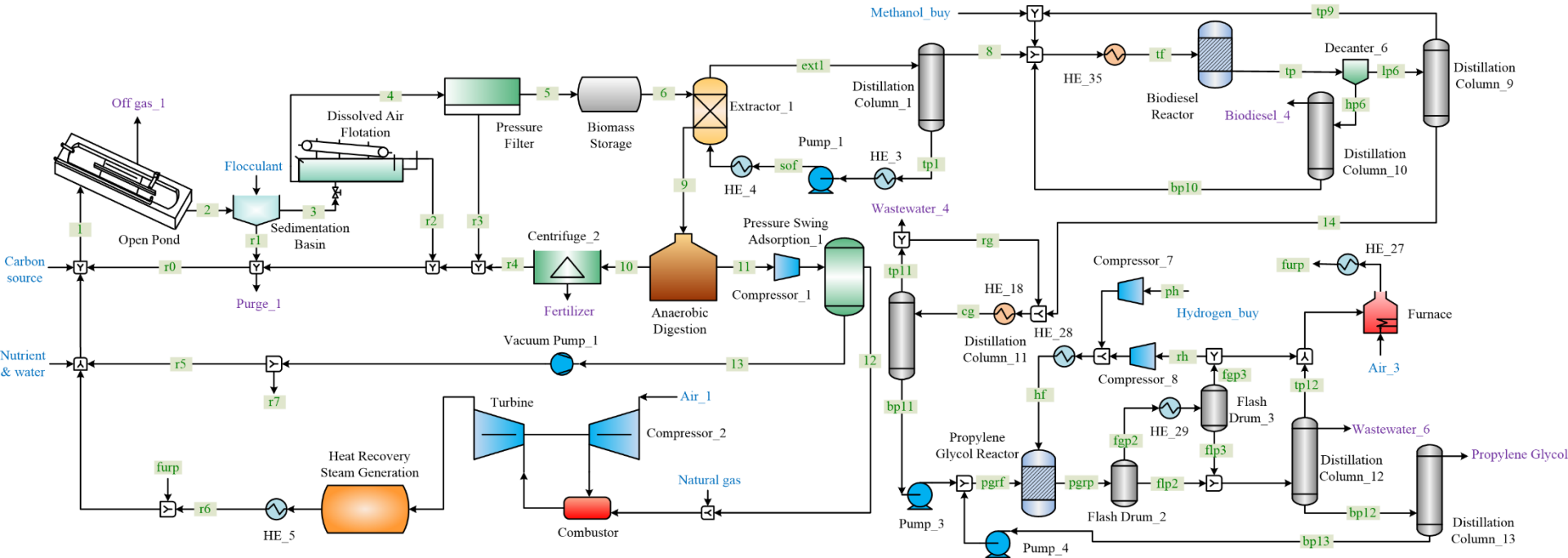
Pareto Optimal Curve



Superstructure of Algae Process



Optimal Design of Minimum Unit Biofuel Cost



Unit cost of biofuel
(\$/GEG)

2.79

Unit GHG emissions
(kg CO₂-eq/GEG)

7.21

Biodiesel
Throughput
(million GGE)

47

Bioproduct

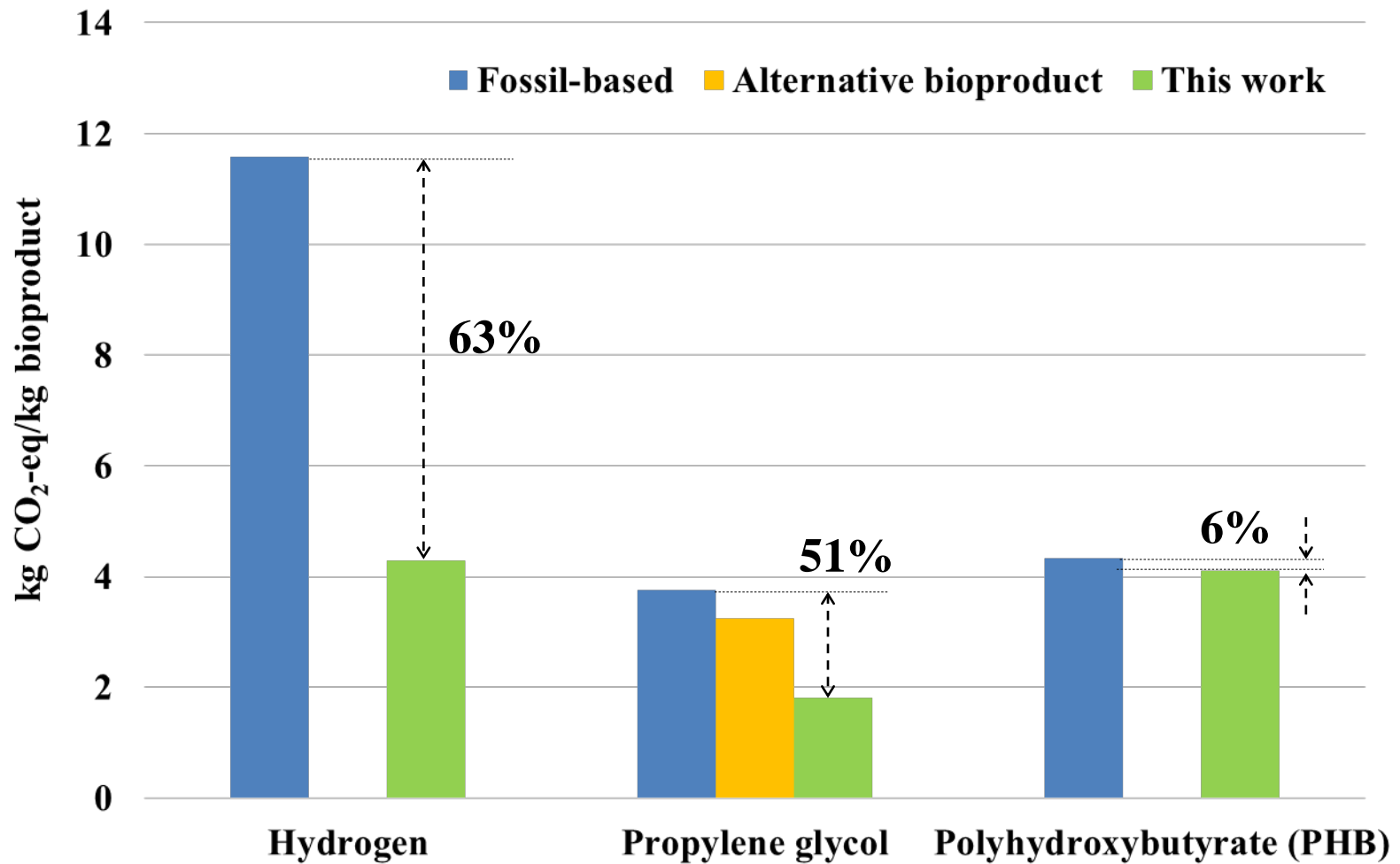
Propylene glycol

2.71 – 3.78

14.43

Petroleum-derived
diesel

GWP of Algae-based H₂, PHB, Propylene Glycol



*Alternative bio-based propylene glycol is derived from **soybean** by ADM(R).*

Value-Added Chemicals from Microalgae: Greener, More Economical, or Both?

Jian Gong and Fengqi You*

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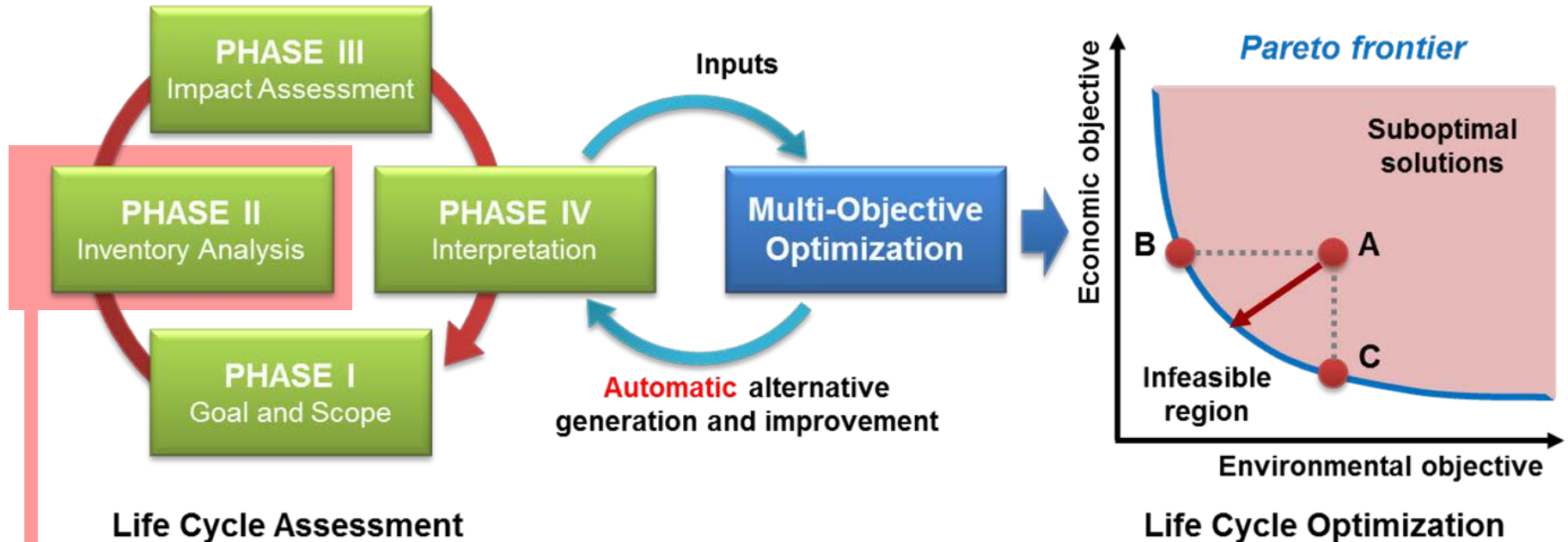
Supporting Information

ABSTRACT: This paper addresses the sustainable design and synthesis of manufacturing processes for making algal bioproducts. We propose by far the most comprehensive superstructure capable of producing biodiesel, hydrogen, propylene glycol, glycerol-*tert*-butyl ether, and poly-3-hydroxybutyrate from microalgae. The major processing sections include cultivation, harvesting, lipid extraction, remnant treatment, biogas utilization, biofuel production, and bioproduct manufacturing. On the basis of the superstructure, we integrate a cradle-to-gate life cycle analysis and techno-economic analysis with multiobjective optimization to simultaneously optimize the environmental and economic performance. We also apply a tailored global optimization algorithm to efficiently solve the problem in reasonable computation times. Results show that the most environmentally sustainable processes reduce life cycle greenhouse gas emissions per kilogram of the algal bioproducts by 5% to 63%, compared with petrochemical counterparts. In addition, the coproduction of value-added bioproducts in the algal glycerol process helps reduce the biodiesel production cost to as low as \$2.79 per gasoline-gallon-equivalent.

KEYWORDS: Life cycle analysis, glycerol, bioproduct, algal biofuels, global optimization



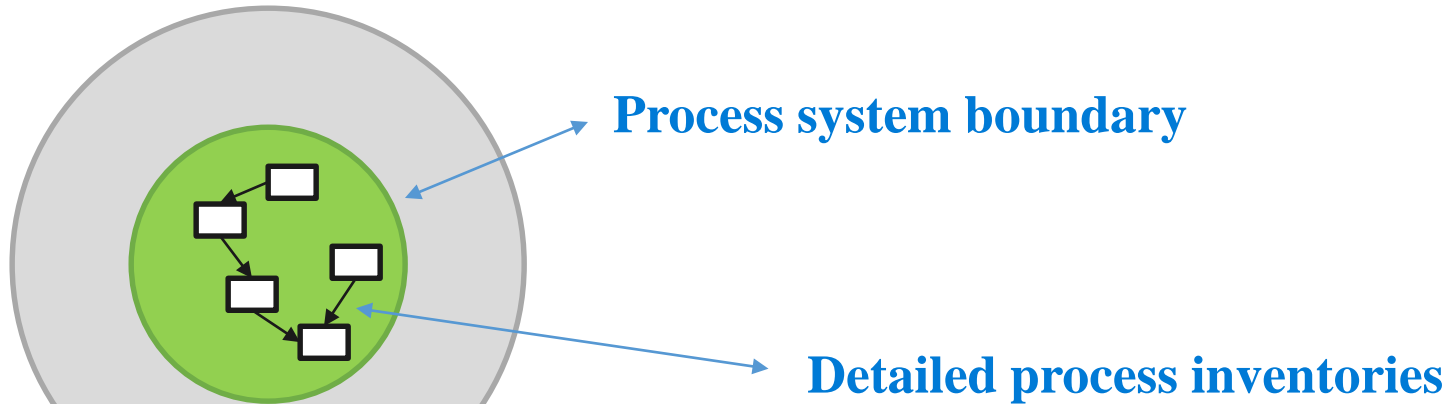
Hybrid Life Cycle Optimization (h-LCO)



Alternative approaches for Life Cycle Inventory (LCI) analysis

- Process-based LCA (most widely used)
- Economic Input-Output (EIO)-based LCA (for macroscopic analysis)
- **Hybrid LCA** (state of the art)

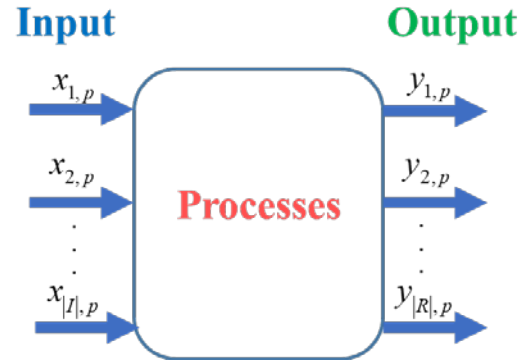
Process-based LCA



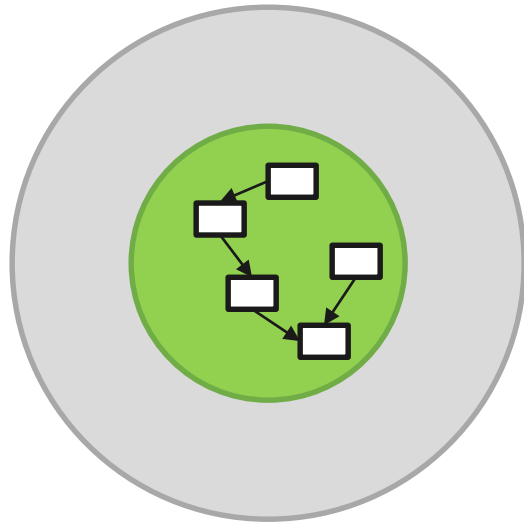
Process-based



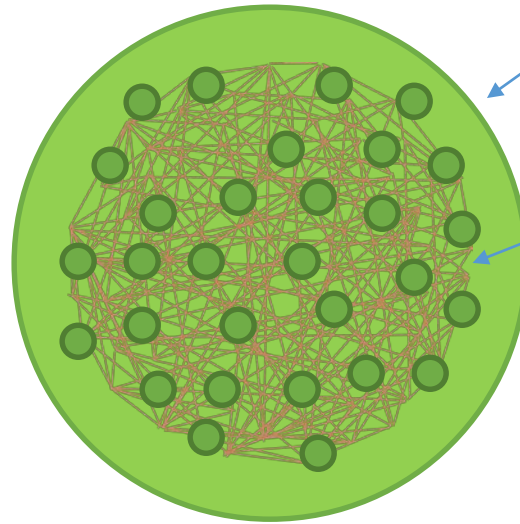
Resolution	Process
Construction	Bottom Up
Scope	Selected Processes



EIO-based LCA



Process-based



EIO-based

Entire macroeconomy

Transactions among sectors

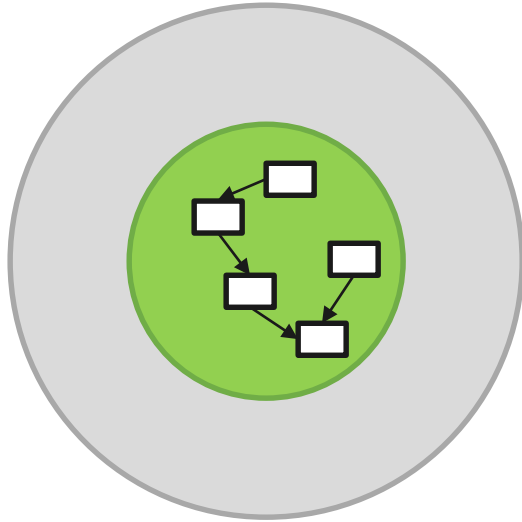
	UK			...	ROW
UK	Sector A ₁	Sector A ₂	...	Sector A _N	
	Sector B ₁	Sector B ₂	...	Sector B _N	
	Sector C ₁	Sector C ₂	...	Sector C _N	
	⋮	⋮	⋮	⋮	
ROW	Sector N ₁	Sector N ₂	...	Sector N _N	

Sectors:

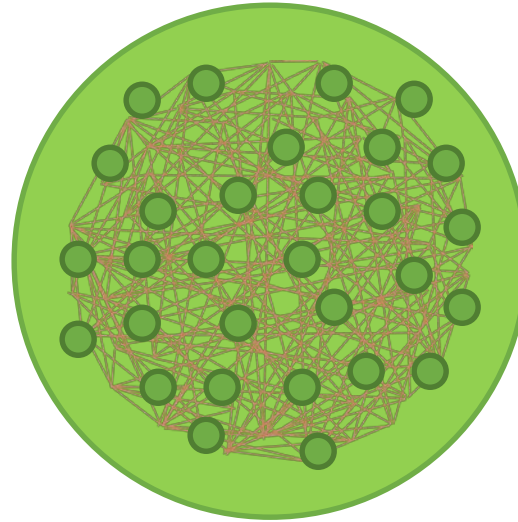
Agriculture, mining, construction, manufacturing, wholesale trade, retail trade, transportation, etc.

Resolution	Process	Sector
Construction	Bottom Up	Top Down
Scope	Selected Processes	Entire Economy

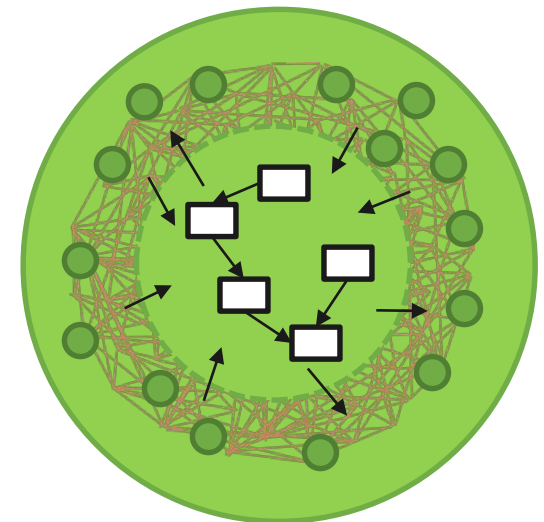
Integrated Hybrid LCA



Process-based



EIO-based



Integrated Hybrid



Resolution	Process	Sector	Process (foreground) Sector (background)
Construction	Bottom Up	Top Down	Hybrid
Scope	Selected Processes	Entire Economy	Entire Economy

Insights into Different LCA Approaches



Drawbacks:

- System boundary truncation
- Underestimation of the true impact

Advantage:

- Specificity of process analysis



Drawbacks:

- Loss of precision at process level

Advantage:

- Completeness of life cycle boundary



Integrates process- and IO-based LCA

Advantages:

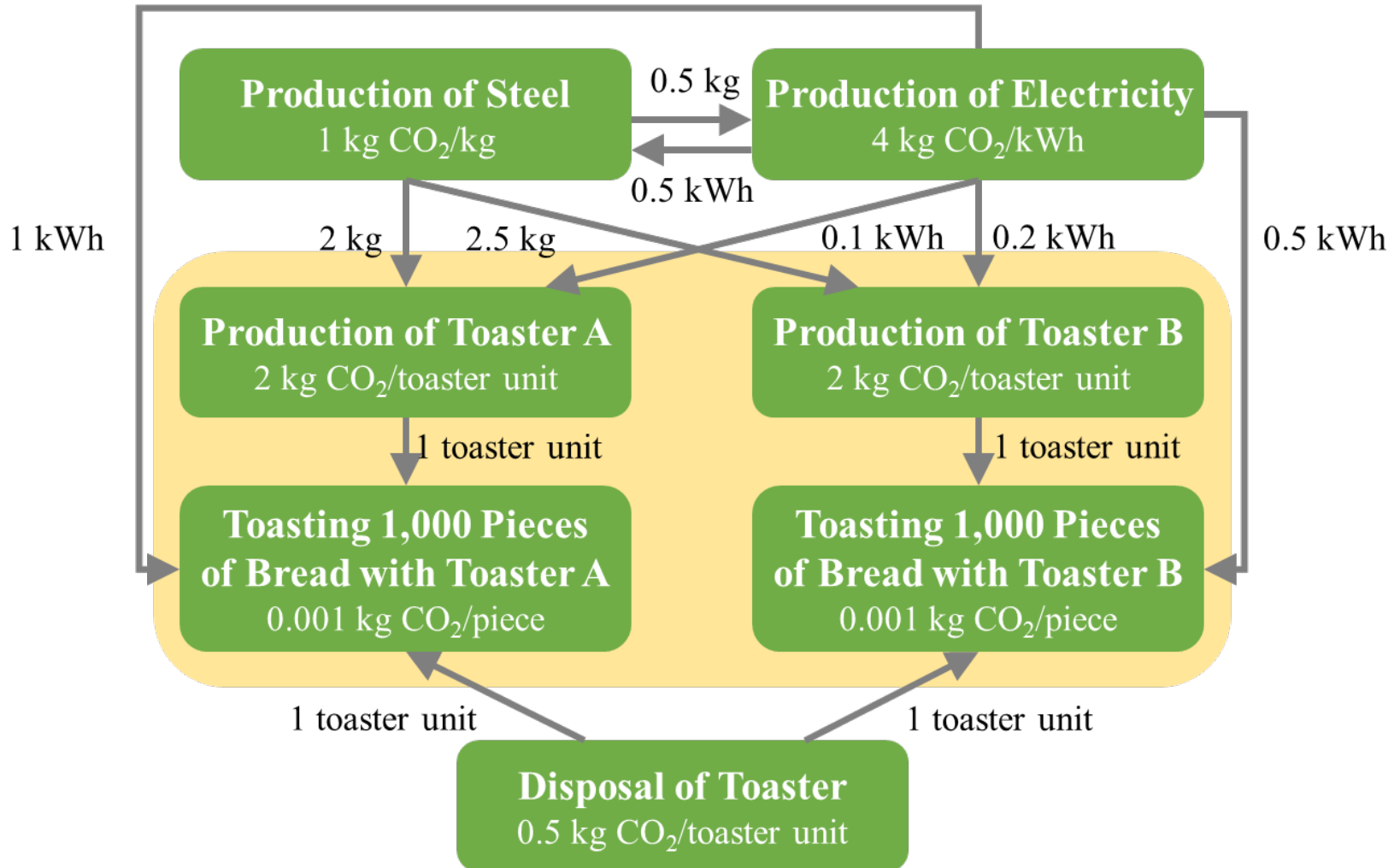
- Completeness of life cycle boundary
- Specificity of foreground processes



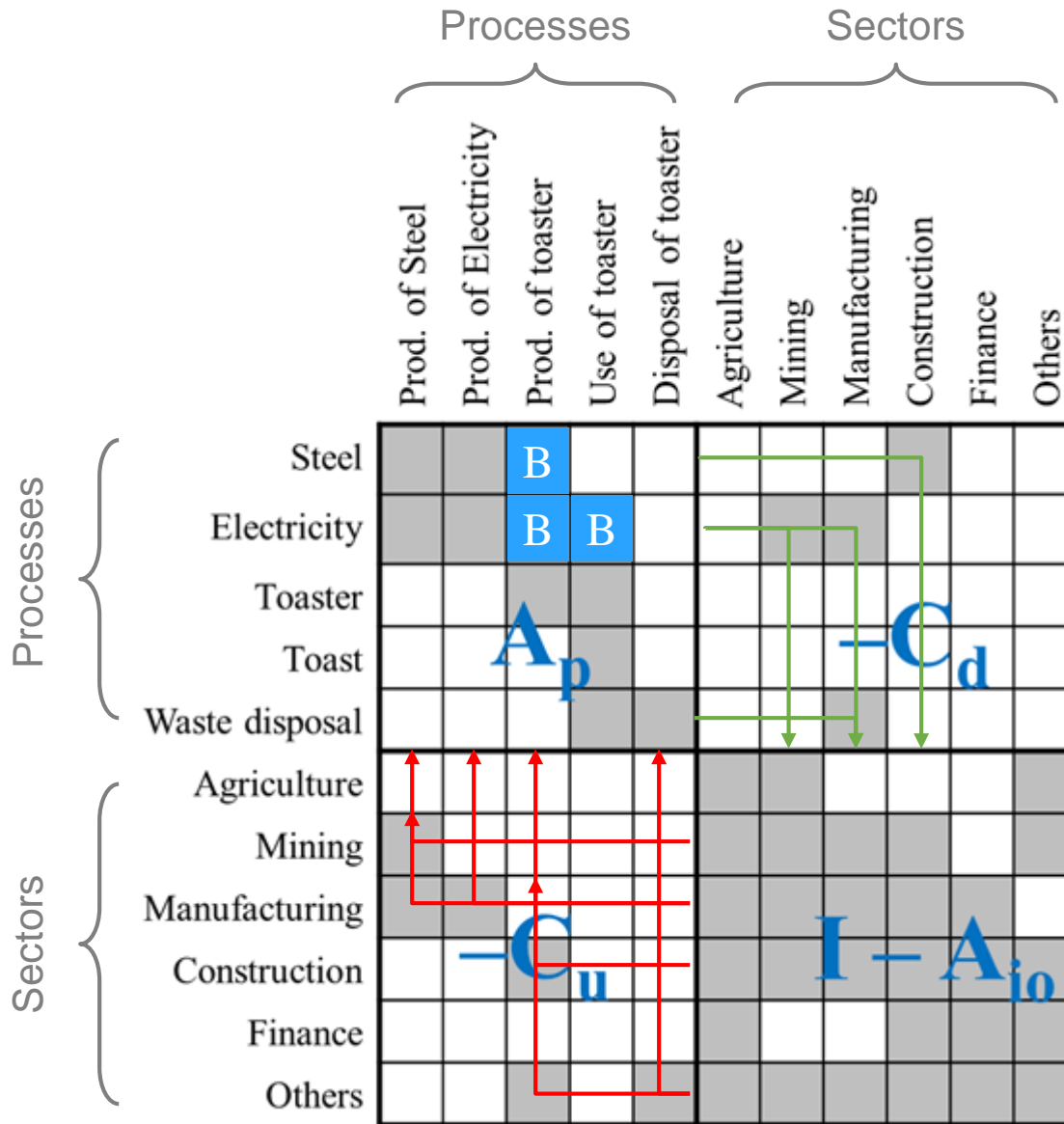
Toaster Example

Comparing two toasters

(Functional unit: produce **1,000** pieces of bread)

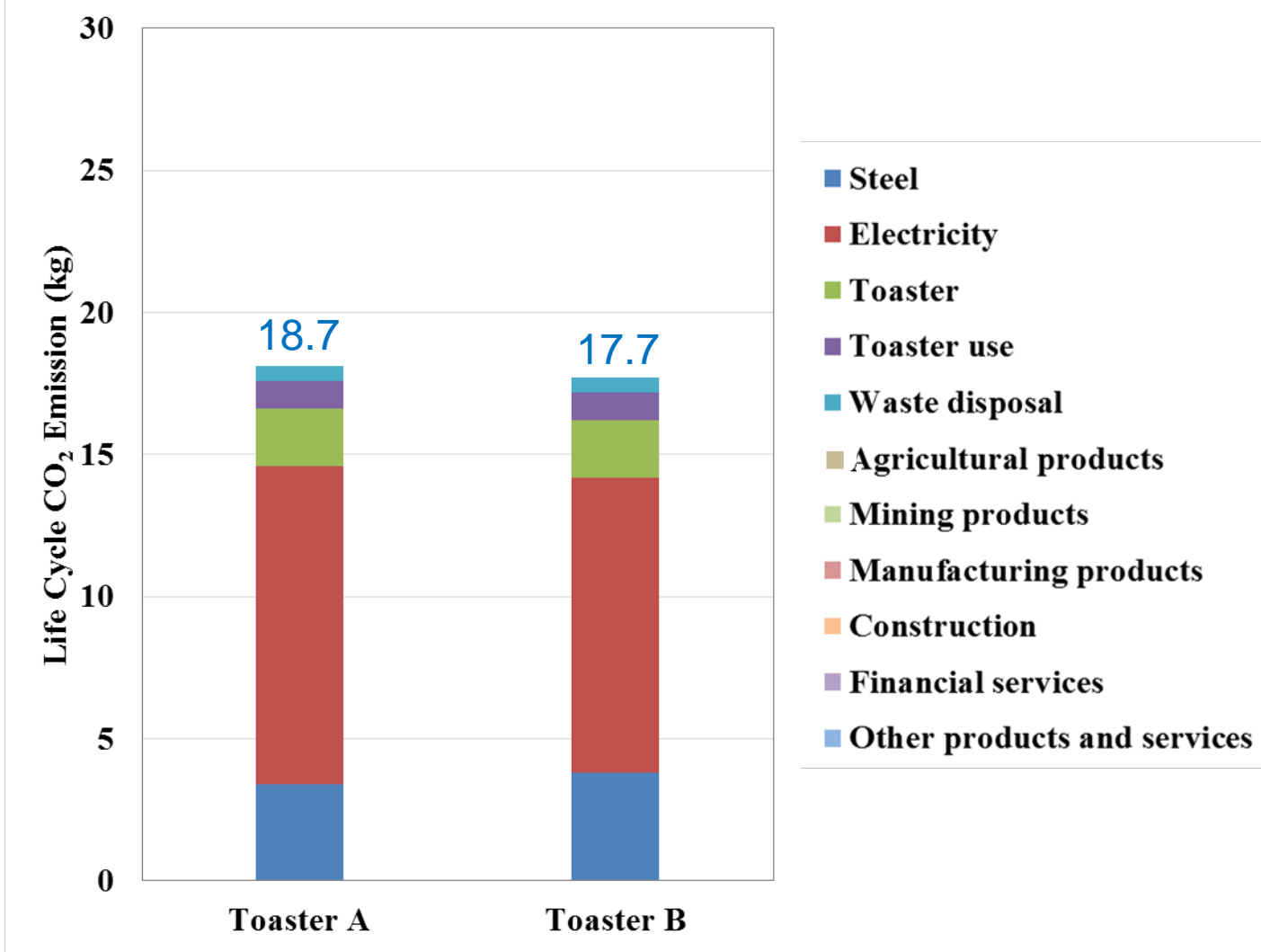


Toaster Example



Toaster Example

Direct emission
(process system)

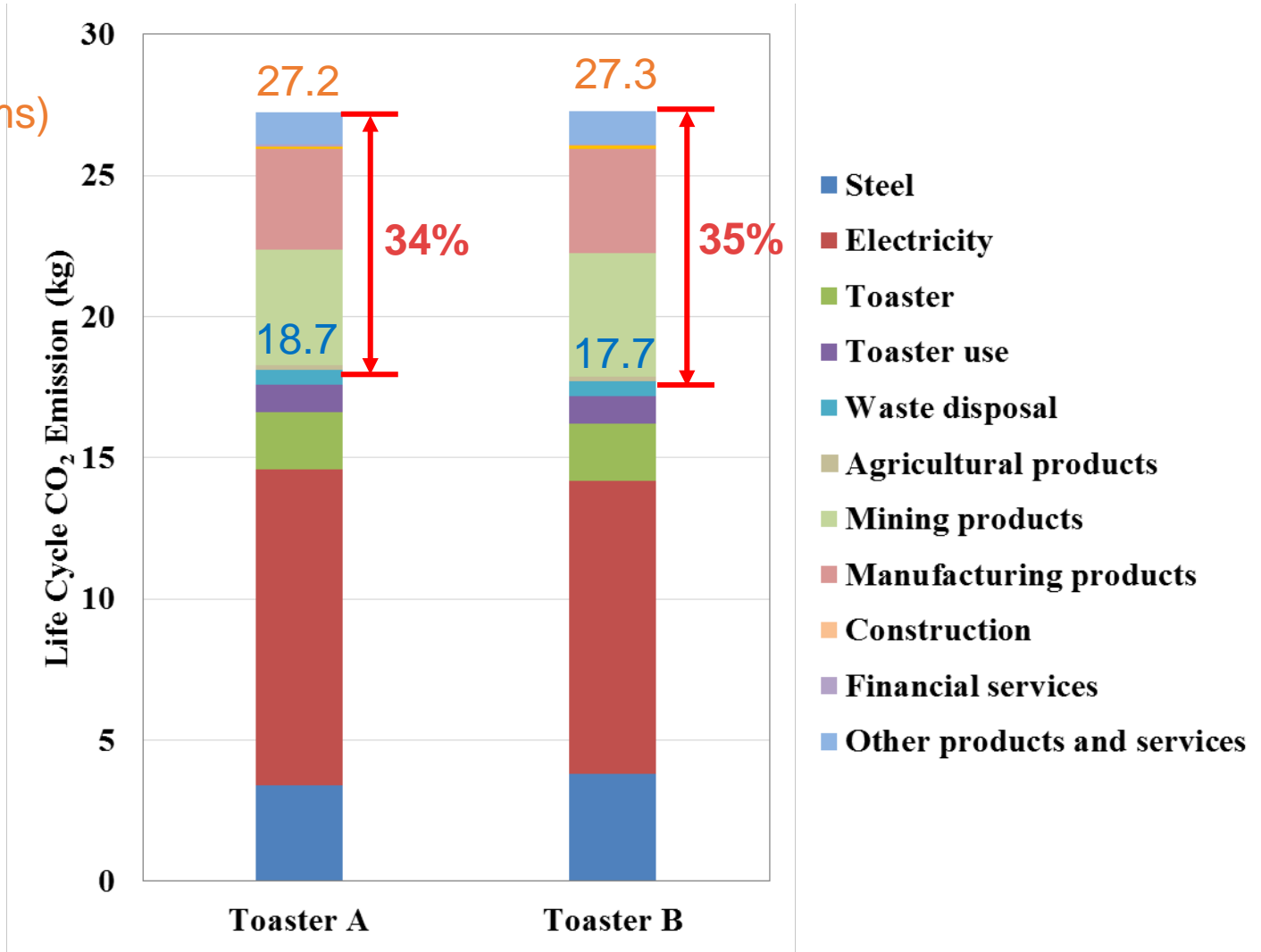


Toaster Example

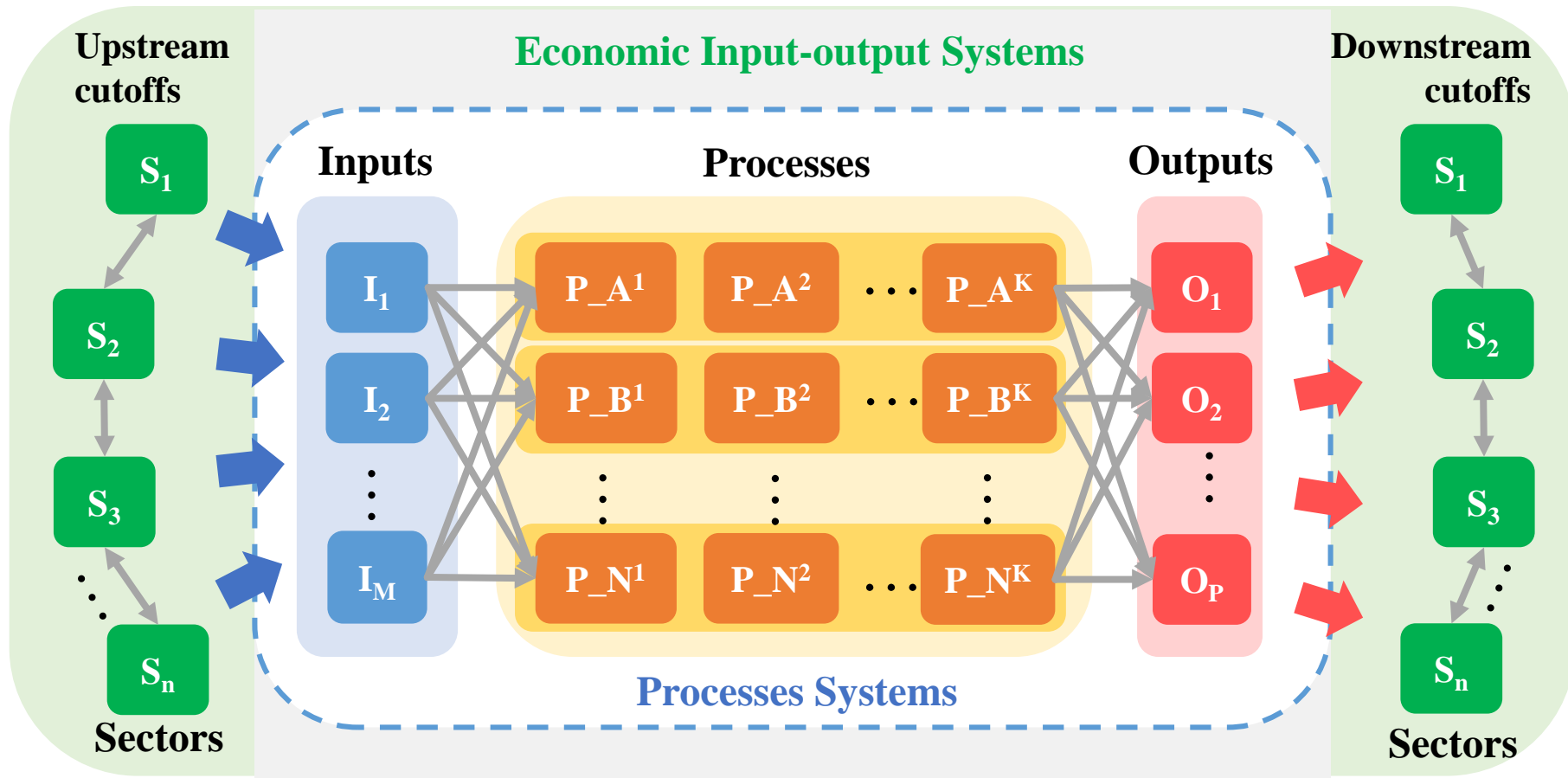
Full emission
(process + IO systems)

Neglected
indirect emission
(IO system)

Direct emission
(process system)



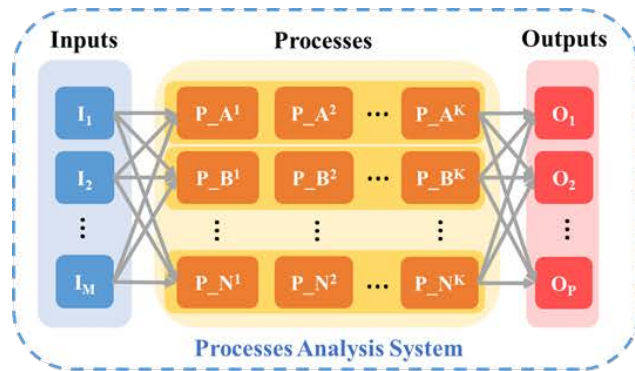
Integrated Hybrid LCA



Integrated Hybrid LCA:

- Explicit process analysis – foreground process systems (precision of analysis)
- EIO analysis – background macroeconomic systems (complement the truncated system boundary)

Mathematical Foundation



E_p Environmental extension factor (process systems)

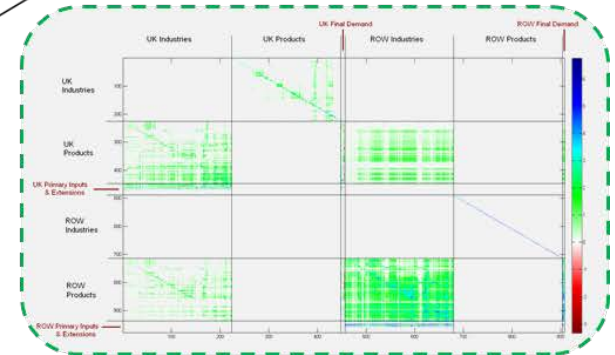
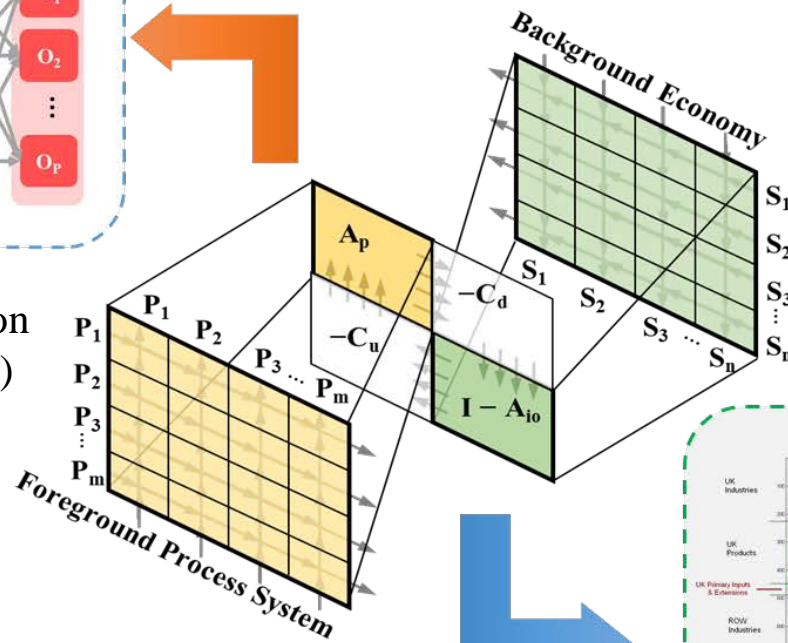
A_p Process matrix

C_u Upstream cutoff matrix

E_{io} Environmental extension factor (EIO systems)

A_{io} Direct requirements matrix

C_d Downstream cutoff matrix

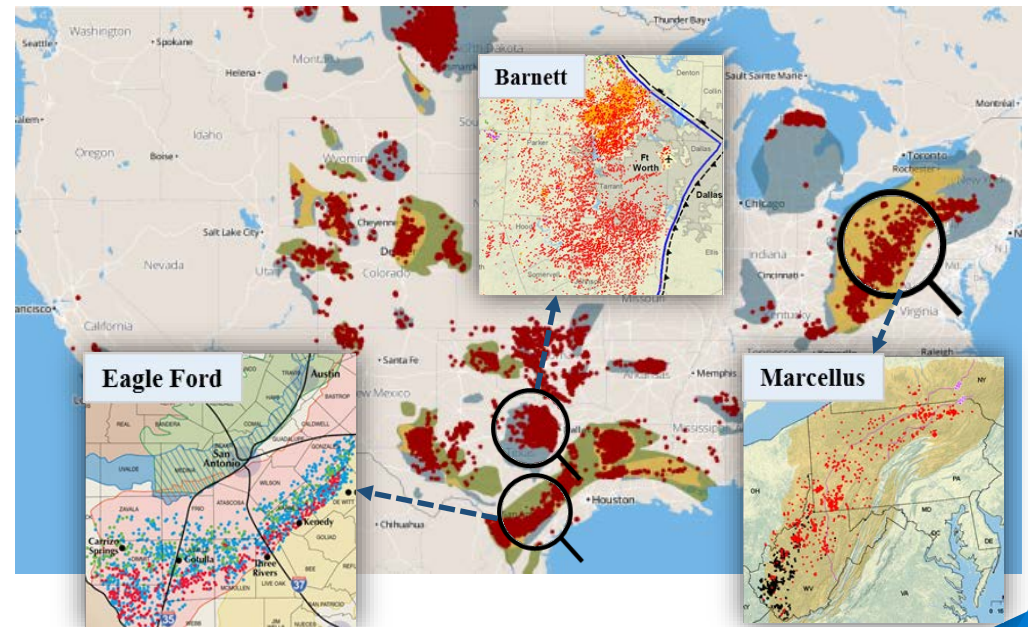
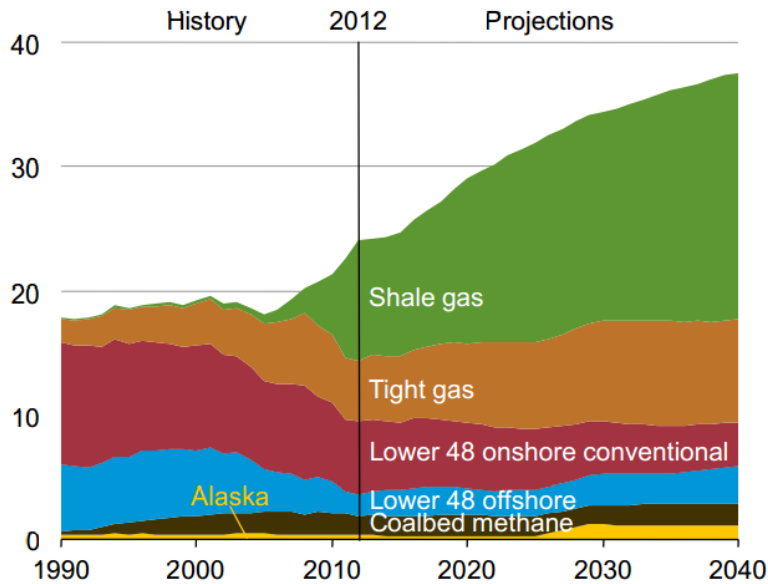


$$\text{Total environmental impact} = \begin{bmatrix} E_p & E_{io} \end{bmatrix} \begin{bmatrix} A_p & -C_d \\ -C_u & I - A_{io} \end{bmatrix}^{-1} \begin{bmatrix} y \\ 0 \end{bmatrix}$$

Application to Shale Gas

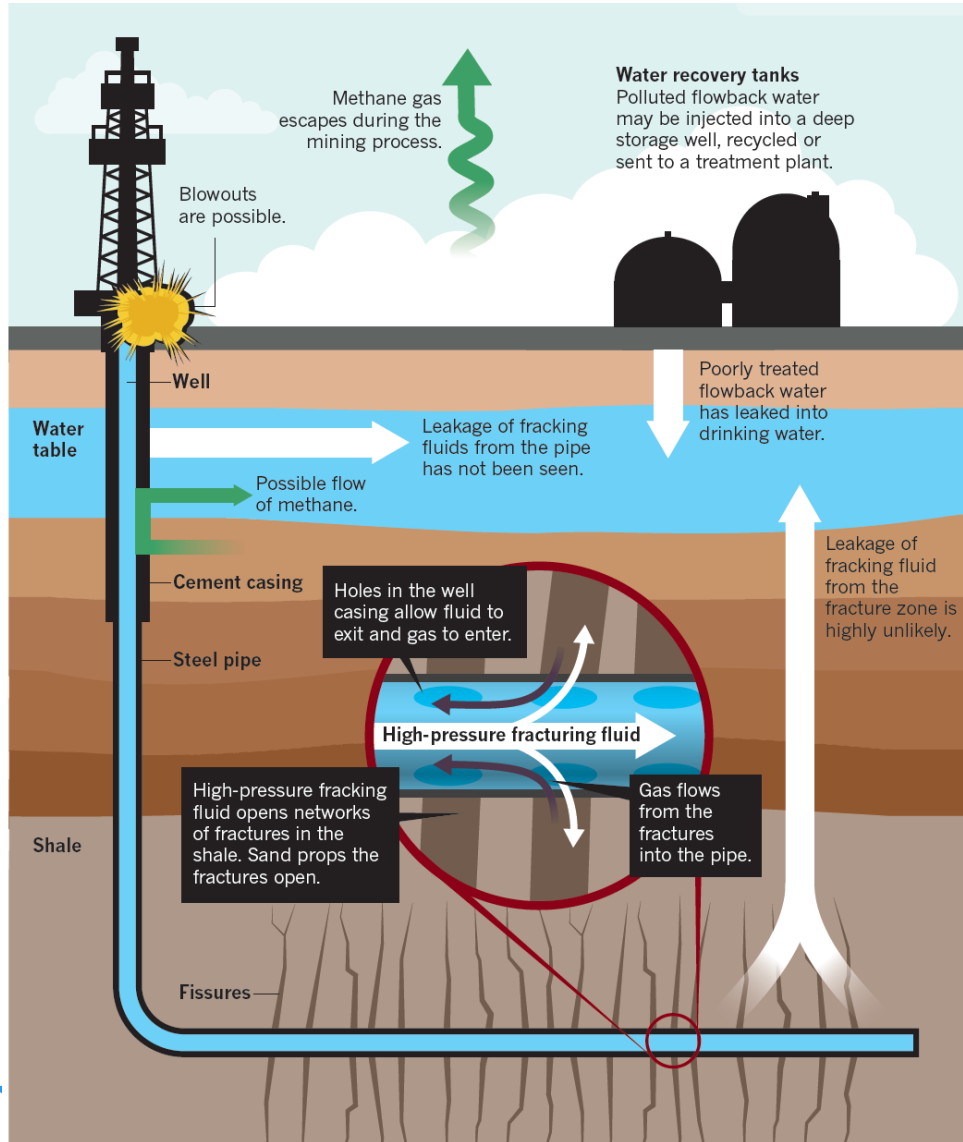


- Unconventional natural gas from shale rocks
- Large-scale production due to **hydraulic fracturing** and **horizontal drilling**
- Half of the NG production in the U.S.
- **Over 63,000 shale wells in the U.S.**

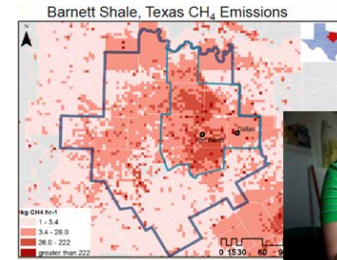


U.S. natural gas production

Hybrid LCA of Shale Gas



Climate change



Lyon et al, 2015.



Water consumption



Other: <2%	Friction Reducer Used in swimming pools
Acid Used in swimming pools	Anti-bacterial Agent Used in disinfectants
Anti-bacterial Agent Used in disinfectants	Broaker Used in hair color
Broaker Used in hair color	Clay Stabilizer Used in IV fluids
Clay Stabilizer Used in IV fluids	Corrosion Inhibitor Used in plastics
Corrosion Inhibitor Used in plastics	Crosslinker Used in laundry detergents
Crosslinker Used in laundry detergents	Friction Reducer Used in cosmetics
Friction Reducer Used in cosmetics	Gelling Agent Used in toothpastes
Gelling Agent Used in toothpastes	Iron Control Used in food additives
Iron Control Used in food additives	pH Adjusting Agent Used in many bar soaps
pH Adjusting Agent Used in many bar soaps	Scale Inhibitor Used in household cleaners
Scale Inhibitor Used in household cleaners	Surfactant Used in deodorant
Surfactant Used in deodorant	

Energy consumption



LCA of Shale Gas

Goal and scope

- **UK** shale gas
- System boundary: **well-to-wire**
- Functional unit: **1 MWh electricity** generation from shale gas



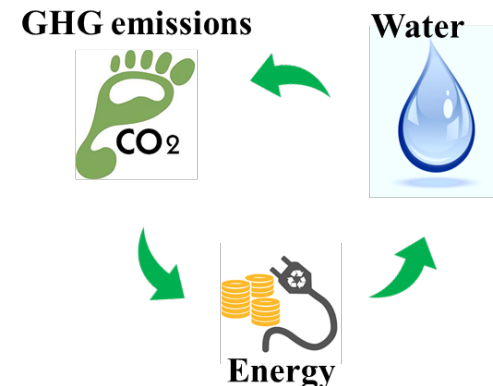
Shale gas

Life cycle inventory

- **40** basic processes in the process systems
- Two-region IO model (UK-ROW) with **224** industrial sectors
- Three cases from literature: **best, balance, and worst** cases corresponding to the **lowest, the medium, and the highest** environmental impacts

Impact assessment

- **GHG** emissions (100-year GWP factors; CO₂, CH₄, N₂O, HFCs, PFCs, and SF₆)
- **Water** consumption
- **Energy** consumption



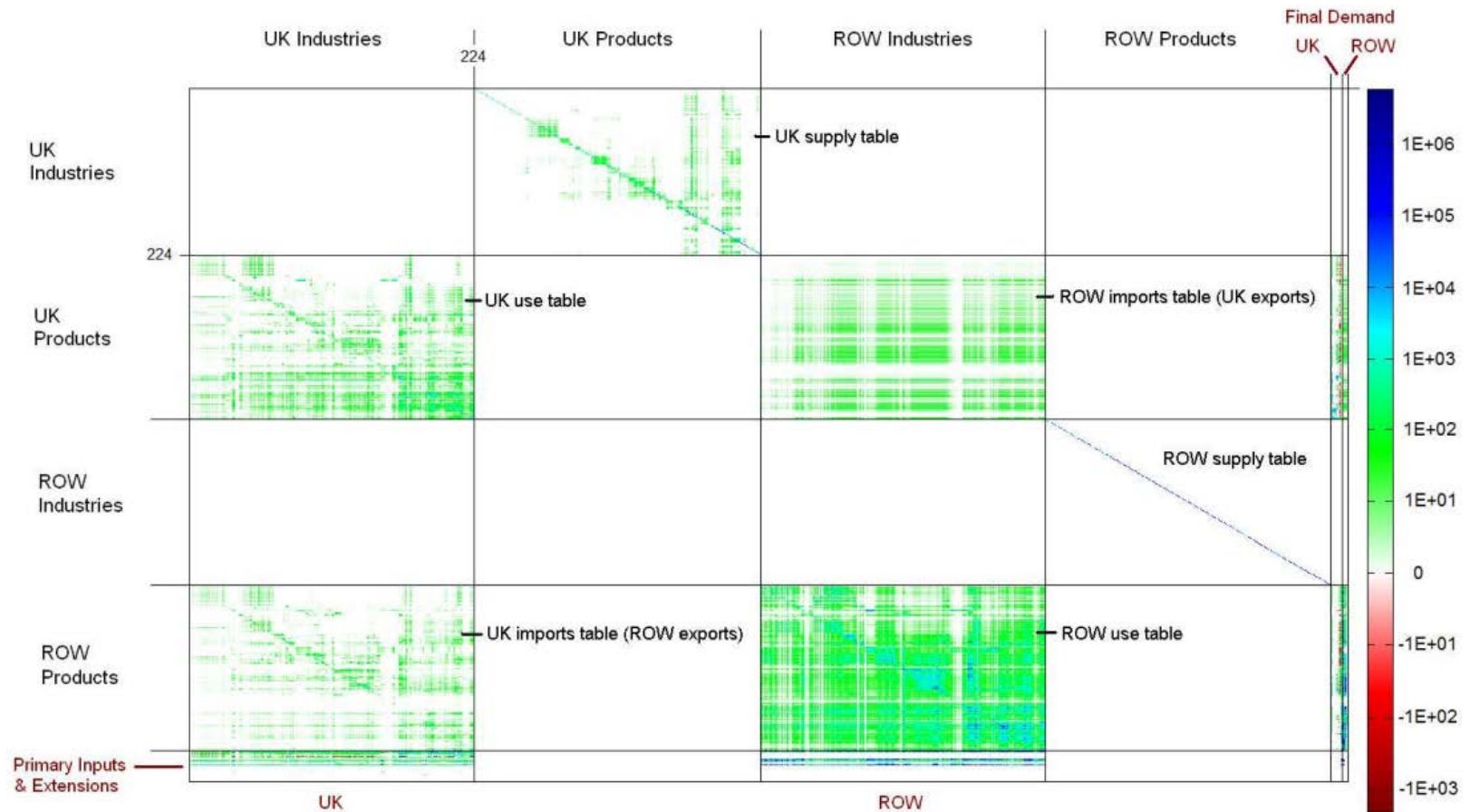
Process Systems – 40 Basic Processes

Process ID	Description	Process ID	Description
m ₁	Steel production, converter, chromium steel 18/8	m ₂₁	Soda ash, dense, to generic market for neutralizing agent
m ₂	Concrete production, for civil engineering, with cement CEM I	m ₂₂	Sodium persulfate production
m ₃	Tap water production, direct filtration treatment	m ₂₃	Sodium borates production
m ₄	Diesel production, low-sulfur	m ₂₄	Citric acid production
m ₅	Diesel, burned in building machine	m ₂₅	Pesticide production, unspecified
m ₆	Diesel, burned in diesel-electric generating set, 18.5kW	m ₂₆	N, N-dimethylformamide production
m ₇	Barite production	m ₂₇	UK electricity generation, with mixed energy inputs
m ₈	Bentonite quarry operation	m ₂₈	Transport, freight, lorry, all sizes, EURO3 to generic market for transport, freight, lorry, unspecified
m ₉	Chemical production, inorganic	m ₂₉	Injection in disposal well
m ₁₀	Chemical production, organic	m ₃₀	Wastewater treatment by CWT
m ₁₁	Lignite mine operation	m ₃₁	Onsite treatment with MSF
m ₁₂	Treatment of inert waste, inert material landfill	m ₃₂	Onsite treatment with MED
m ₁₃	Treatment of drilling waste, landfarming	m ₃₃	Onsite treatment- with RO
m ₁₄	Silica sand production	m ₃₄	Steam production, in chemical industry
m ₁₅	Petroleum refinery operation	m ₃₅	Tap water production, direct filtration treatment
m ₁₆	Isopropanol production	m ₃₆	Transporting gas through pipelines
m ₁₇	Hydrochloric acid production, from the reaction of hydrogen with chlorine	m ₃₇	Ethanolamine production
m ₁₈	Ethylene glycol production	m ₃₈	Ethylene glycol production
m ₁₉	Potassium chloride production	m ₃₉	Fugitive emissions of CO ₂
m ₂₀	Carboxymethyl cellulose production, powder	m ₄₀	Fugitive emissions of CH ₄

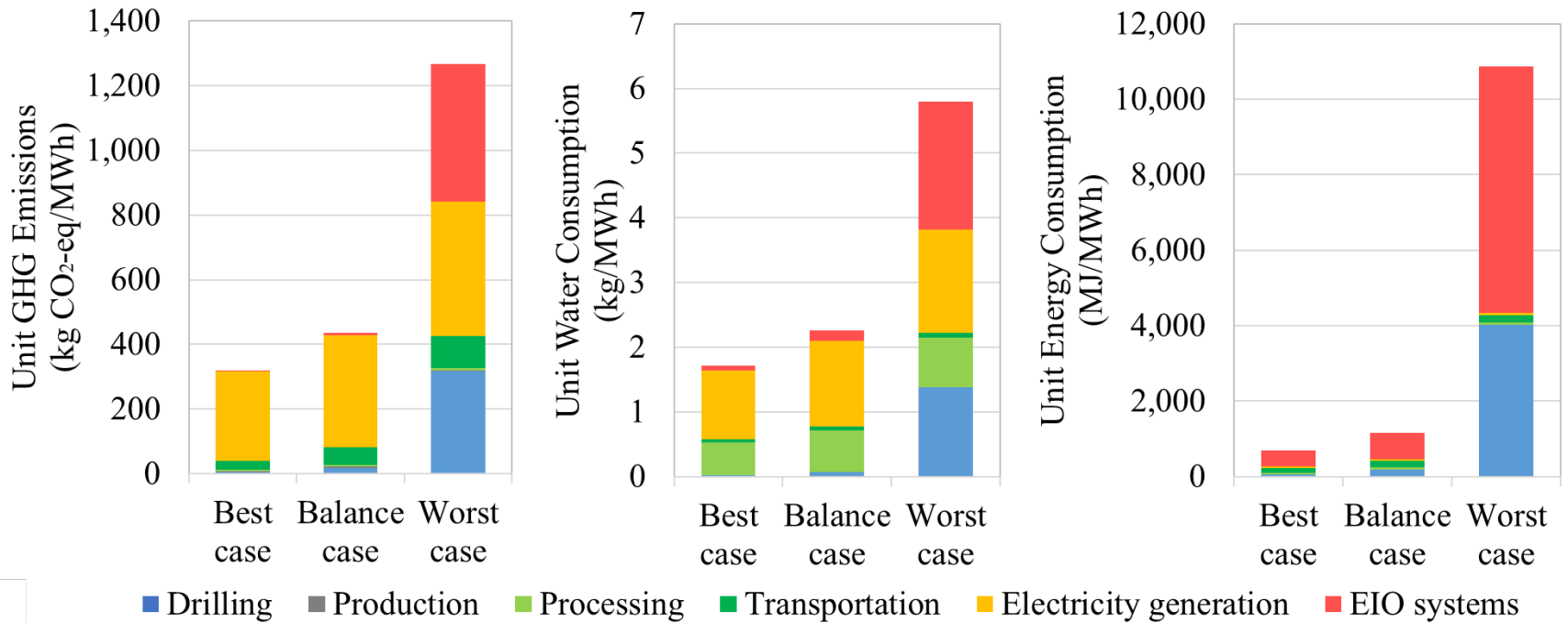
Hybrid LCI Data Structure

IO System (896 × 896 matrix)

- Multi-region: UK and ROW (rest of world)
- Supply-Use Table (SUT): each containing 224 industrial sectors/products



LCA Results



- Electricity generation
- Transportation

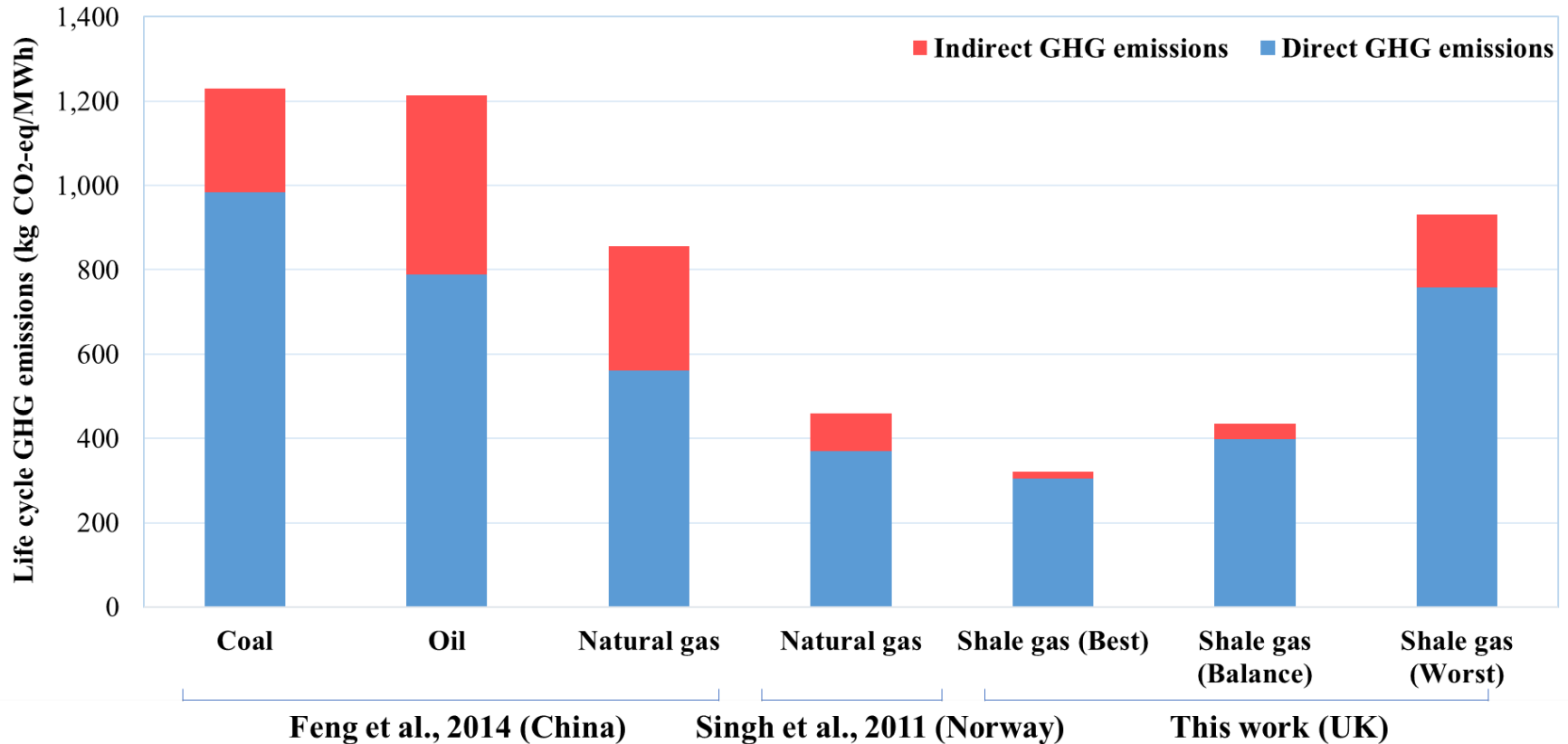


- Electricity generation
- Processing



- Drilling
- EIO system

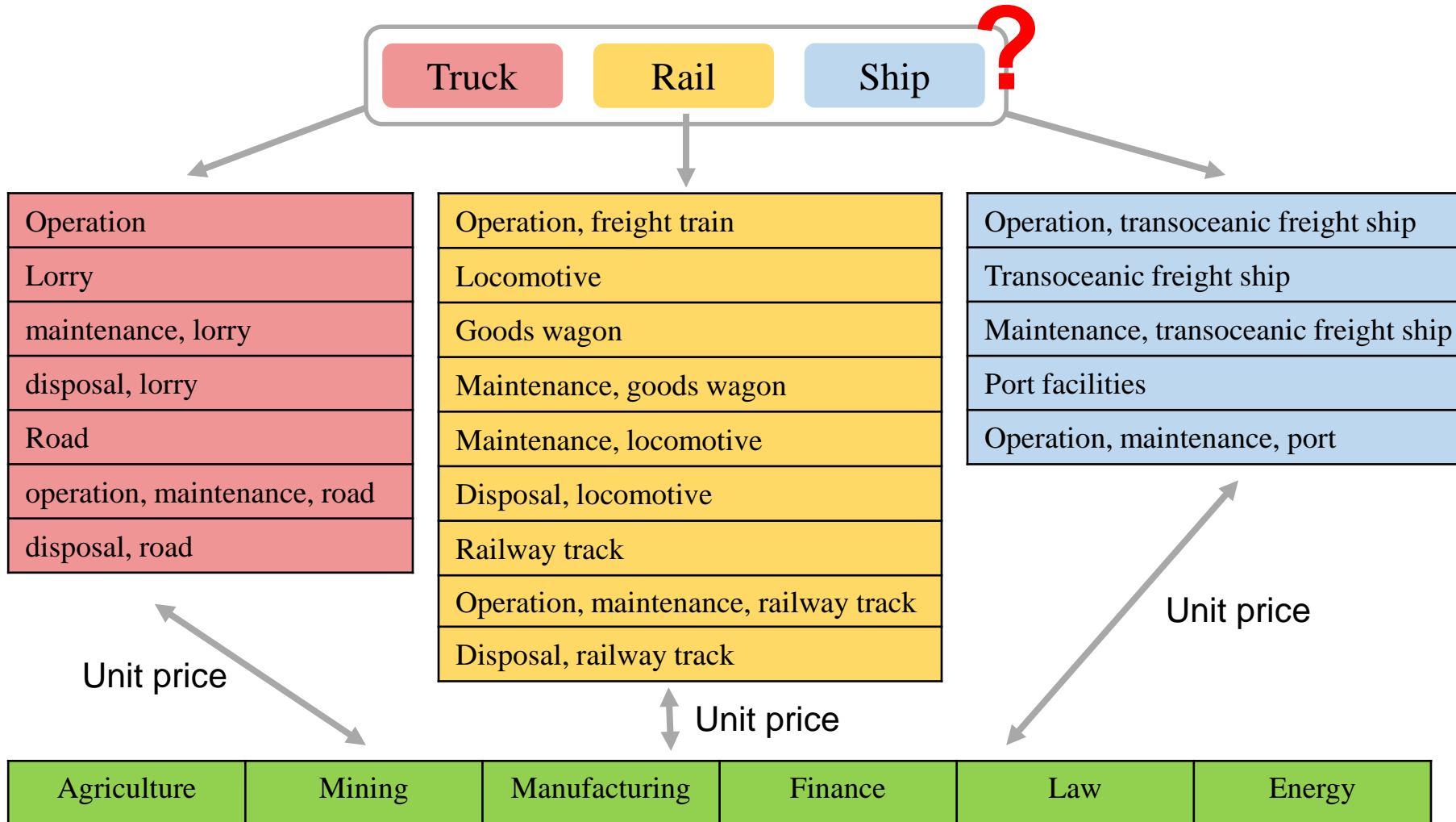
Comparison with Existing Hybrid LCA Studies



- GHG emissions of shale gas are comparable to those of natural gas
- Less GHG emissions than Coal and Oil

Activity – Linking SC Decisions with h-LCO

Definition: *Activity* is a flexible process that involves decision making.



Hybrid LCO Model for Shale Gas

Economic objective:

$$\min LCOE = \frac{TC^{cap} + \sum_{t \in T} \frac{TC^{oper}}{(1+dr)^t}}{TGE}$$

Nonlinear term:

Environmental objective:

$$\min UE = \frac{TE^{pro} + TE^{IO}}{TGE}$$

$$C_{proc}^{cap} = \sum_{p \in P_n} pri \cdot \left(\frac{PC_p}{prc} \right)^{sfp} \cdot \left(\frac{pci}{rpci} \right)$$

s.t. Economic Constraints

Total GHG emissions :

Environmental Constraints

$$TE^{pro} = e_m^{pro} Q_m \quad TE^{IO} = e_{ns}^{IO} P_{ns}$$

Mass Balance Constraints

Total output of each industrial sector P_{ns}

Capacity Constraints

Composition Constraints

$$P_{ns} - \sum_{ns' \in NS} aio_{ns,ns'} \cdot P_{ns'} \geq UP_{ns}$$

Bounding Constraints

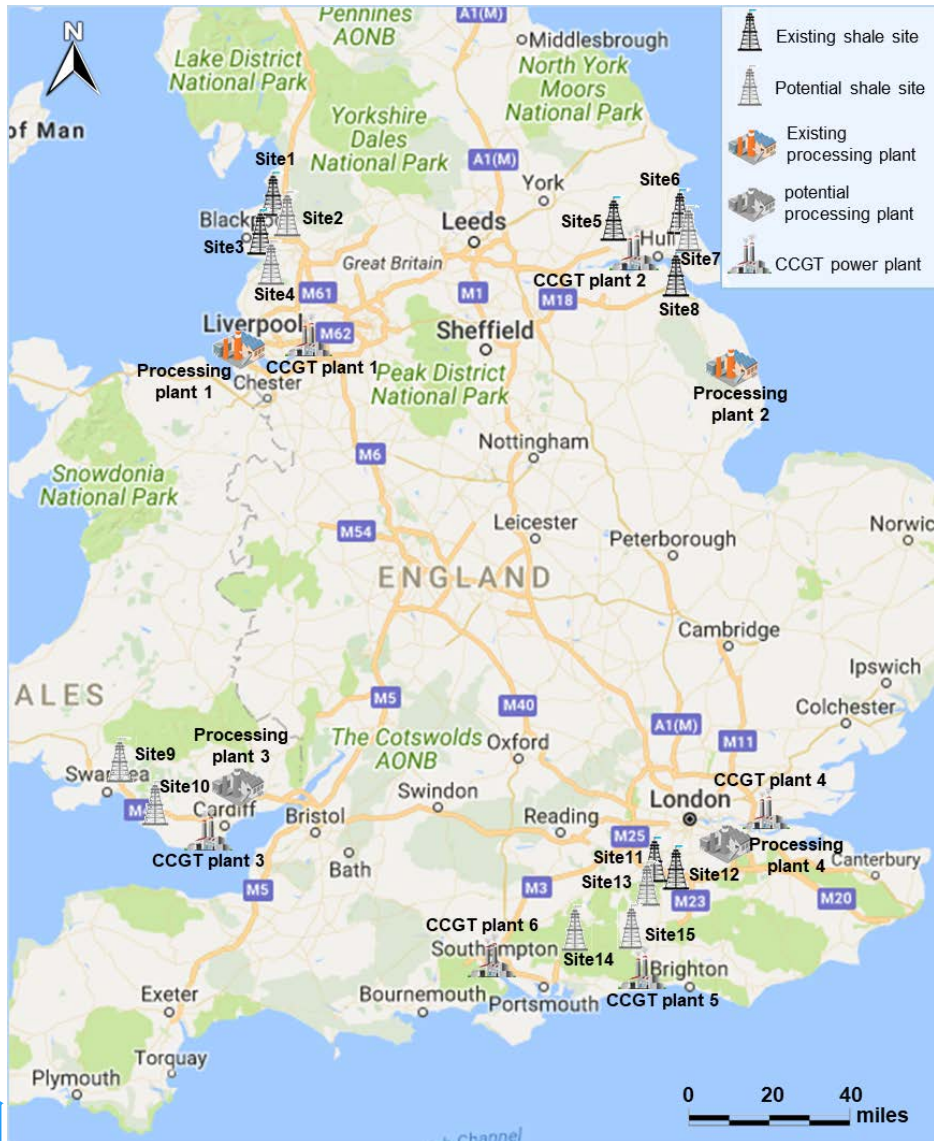
Upstream input from industry sector ns to process systems

Logic Constraints

$$UP_{ns} = \sum_{m \in M} c_{ns,m} \cdot price_m \cdot Q_m$$

Mixed-Integer Nonlinear Fractional Program

Case Study of UK Shale Gas Supply Chain



- **15 Shale sites**
(7 existing, 8 potential ones)

- **4 processing plants**
(2 existing, 2 potential)

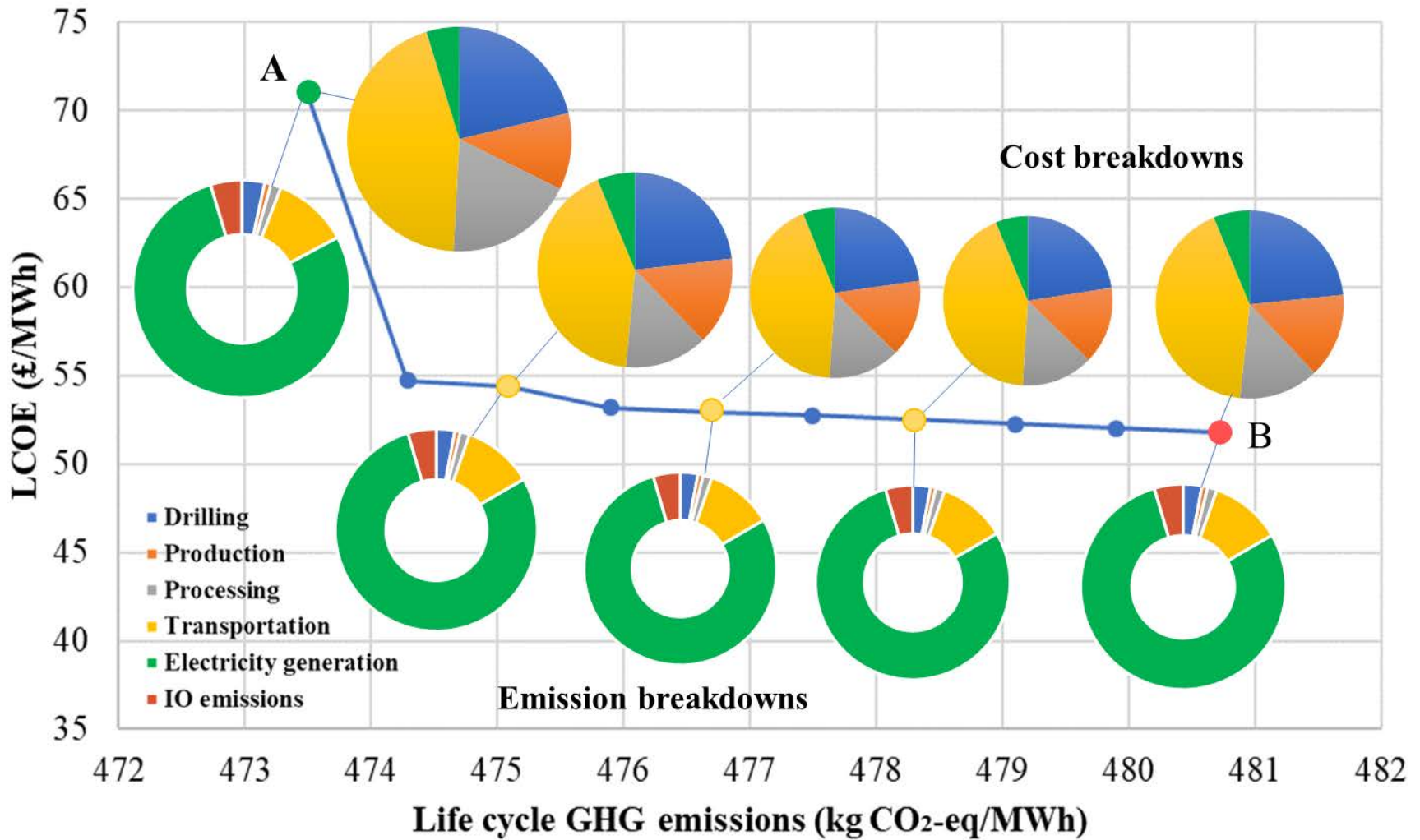
- **6 CCGT power plants**

- **10-year planning horizon**
(40 time periods)

MINLP problem:

- 414 integer variables
- 11,797 continuous variables
- 15,370 constraints

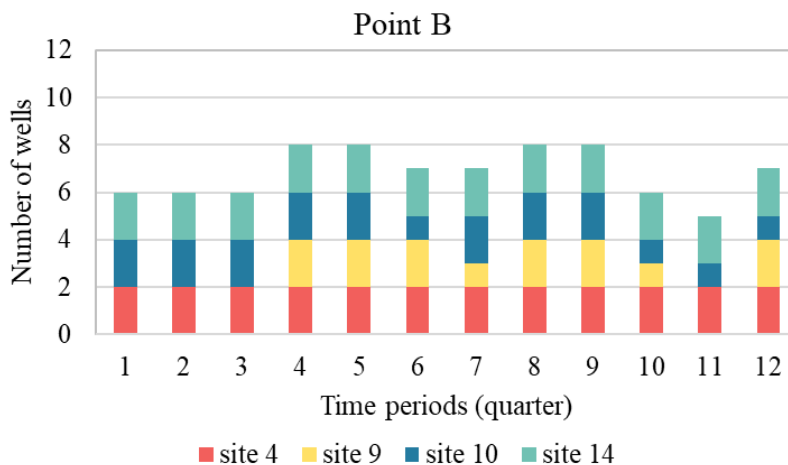
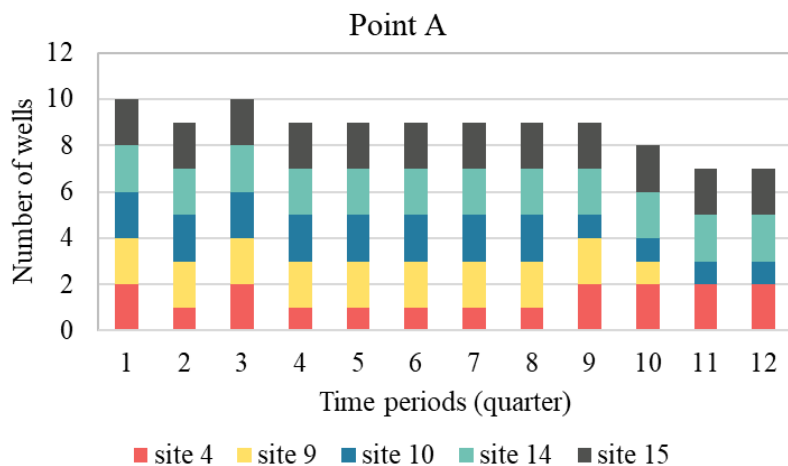
Pareto-optimal Curve



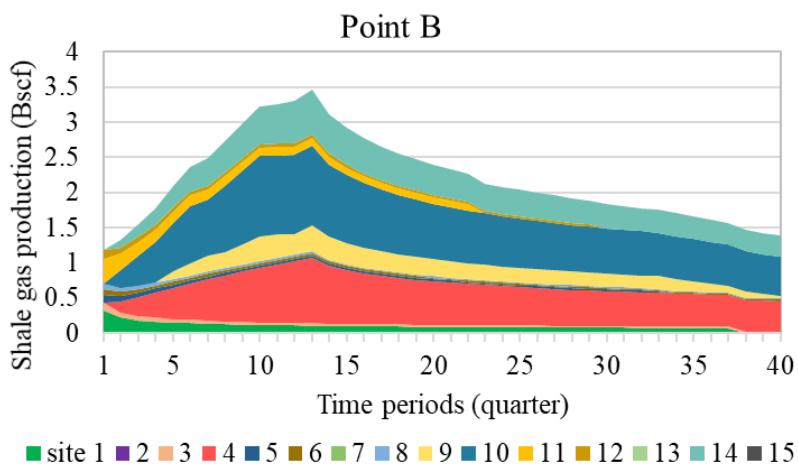
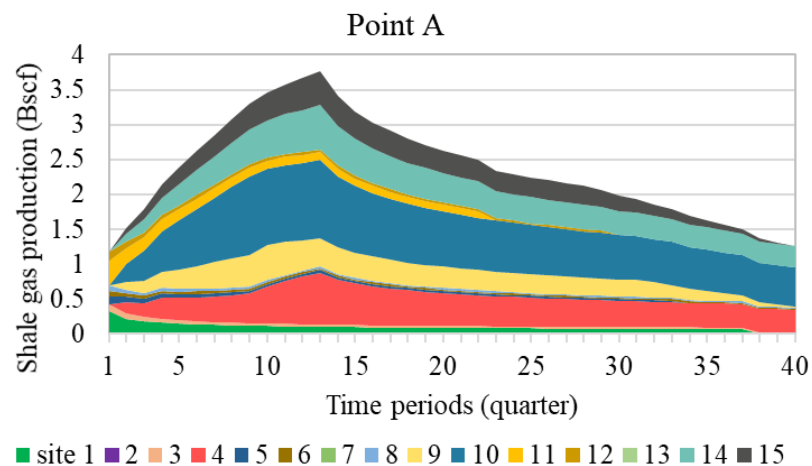
Drilling Schedules and Production Profiles



Drilling Schedules



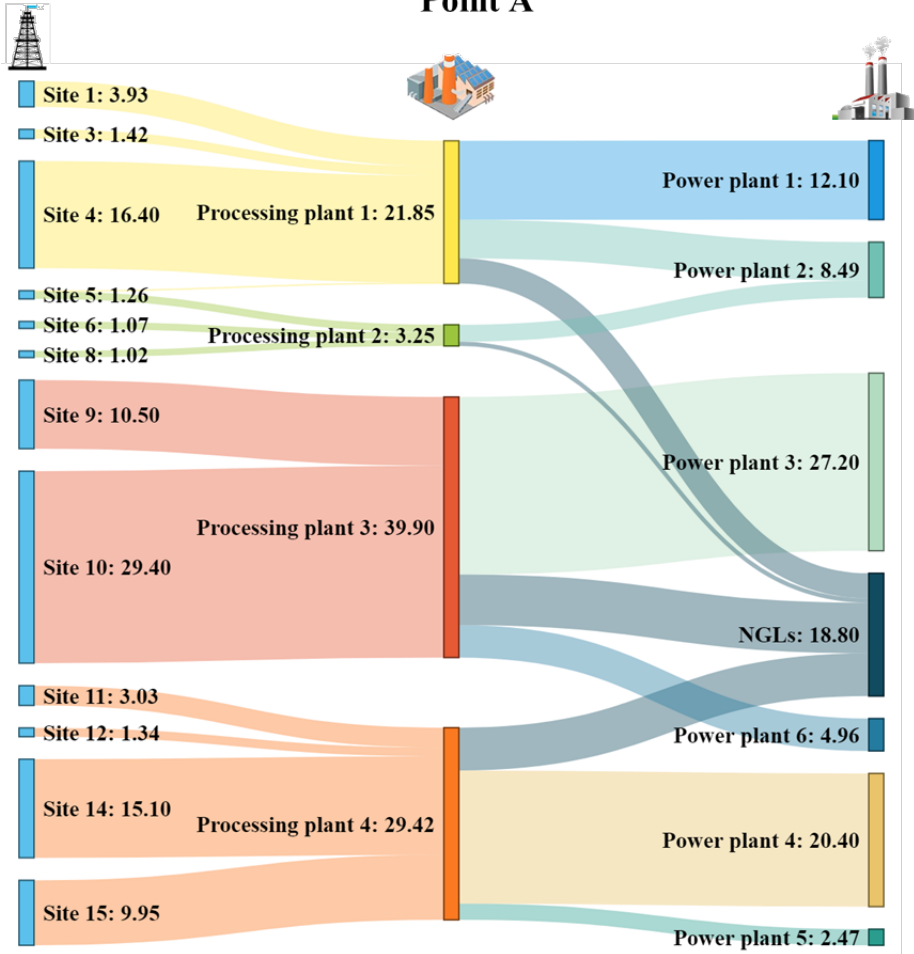
Production Profiles



Supply Chain Design and Flow Information

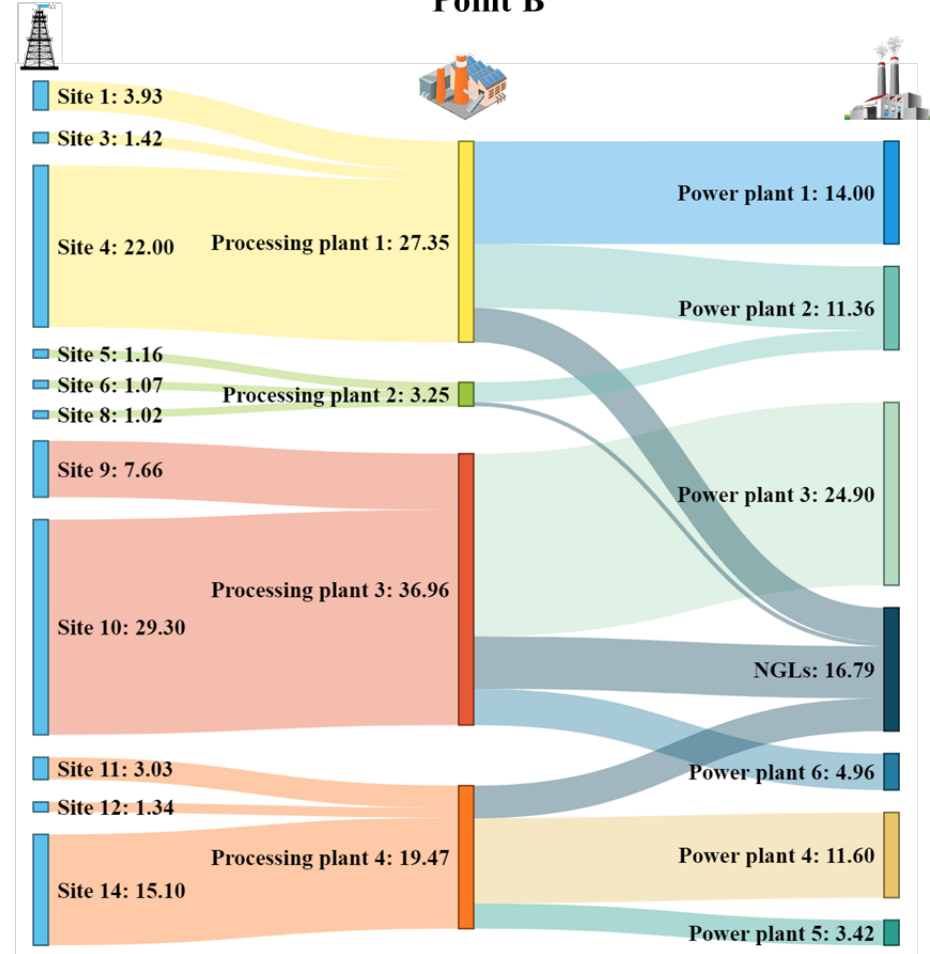


Point A



Unit: Bscf

Point B



Unit: Bscf

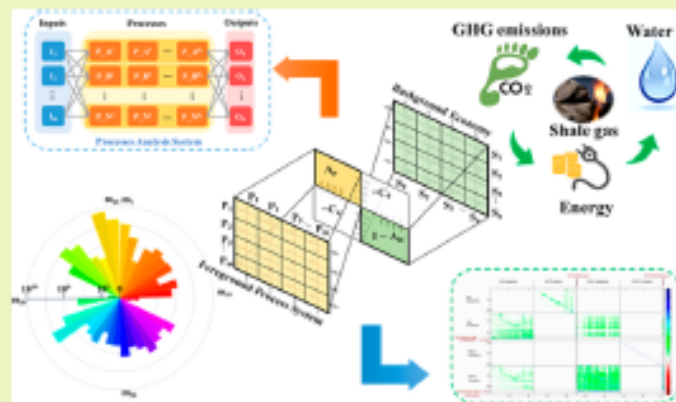
Integrated Hybrid Life Cycle Assessment and Optimization of Shale Gas

Jiyao Gao and Fengqi You*^{ORCID}

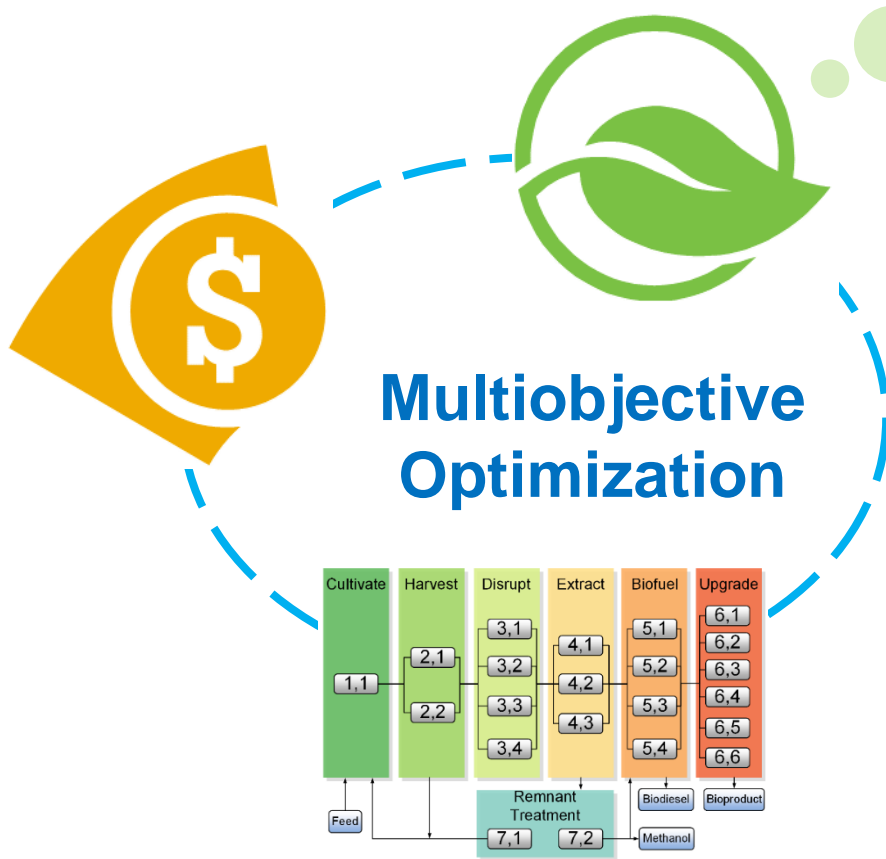
Robert Frederick Smith School of Chemical and Biomolecular Engineering, Cornell University, Ithaca, New York 14853, United States

ABSTRACT: This paper analyzes the life cycle environmental impacts of shale gas by using an integrated hybrid life cycle analysis (LCA) and optimization approach. Unlike the process-based LCA that suffers system truncation, the integrated hybrid LCA supplements the truncated system with a comprehensive economic input-output system. Compared with the economic input-output-based LCA that loses accuracy from process aggregation, the integrated hybrid LCA retains the precision in modeling major unit processes within the well-to-wire system boundary. Three environmental categories, namely, life cycle greenhouse gas emissions, water consumption, and energy consumption, are considered. Based on this integrated hybrid LCA framework, we further developed an integrated hybrid life cycle optimization model, which enables automatic identification of sustainable alternatives in the design and operations of shale gas supply chains. We applied the model to a well-to-wire shale gas supply chain in the UK to illustrate the applicability. According to the optimization results, the lowest levelized cost of electricity generated from shale gas is £51.8/MWh, and the optimal life cycle GHG emissions, water consumption, and energy consumption are 473.5 kg CO₂-eq/MWh, 2263 kg/MWh, and 1009 MJ/MWh, respectively.

KEYWORDS: Hybrid life cycle assessment, Hybrid life cycle optimization, Shale gas, Supply chain



LCO: Attributional v.s. Consequential



Automatic generation of system design decisions

Life Cycle Assessment

Goal and Scope Definition

Life Cycle Inventory Analysis

Life Cycle Impact Assessment

Interpretation

- **Attributional LCA**
- **Consequential LCA**

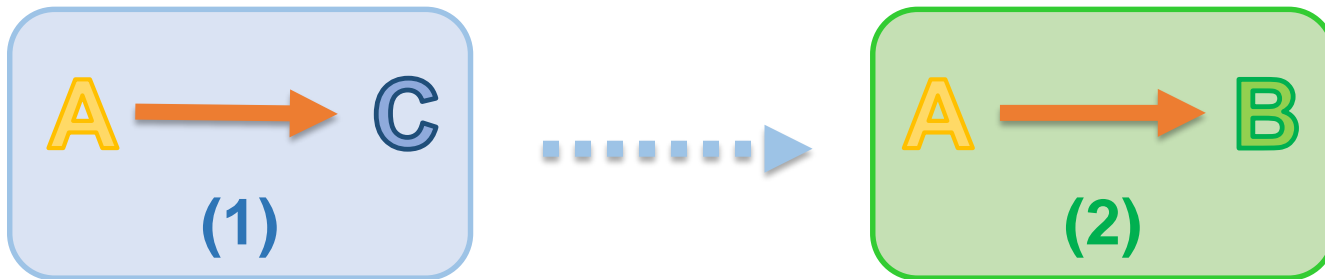
Motivating Example

Attributional LCA: static and fact-based



Environmental Impacts of producing A + Environmental Impacts of the conversion + Environmental Impacts of end of life of B

Consequential LCA: dynamic and change-driven



Environmental Impacts of the new system

-

Environmental Impacts of the original system

Or

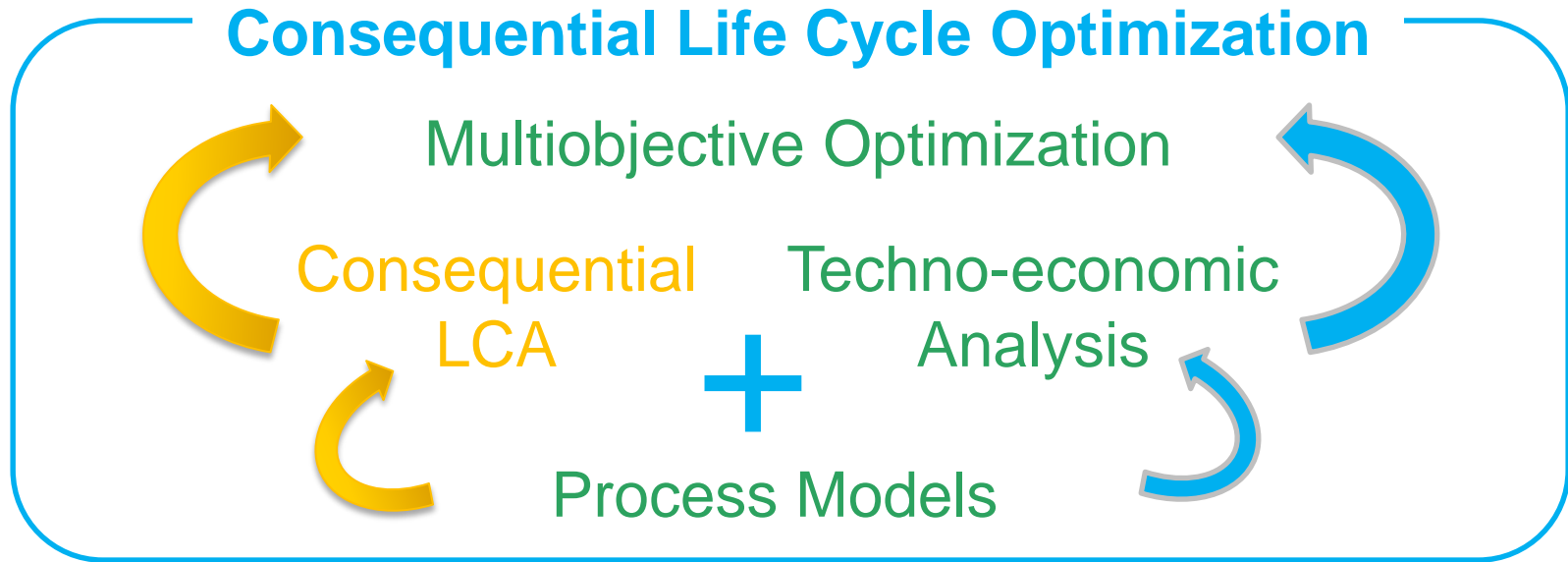
Environmental Impacts of conversion (2) +

Environmental Impacts of end of life of B -

Environmental Impacts of conversion (1) -

Environmental Impacts of end of life of C

Consequential Life Cycle Optimization



How does it work?

- What upstream and downstream processes are influenced by the target process?
- How does the target process influence the upstream and downstream processes?

An Analogy – Spot the Difference

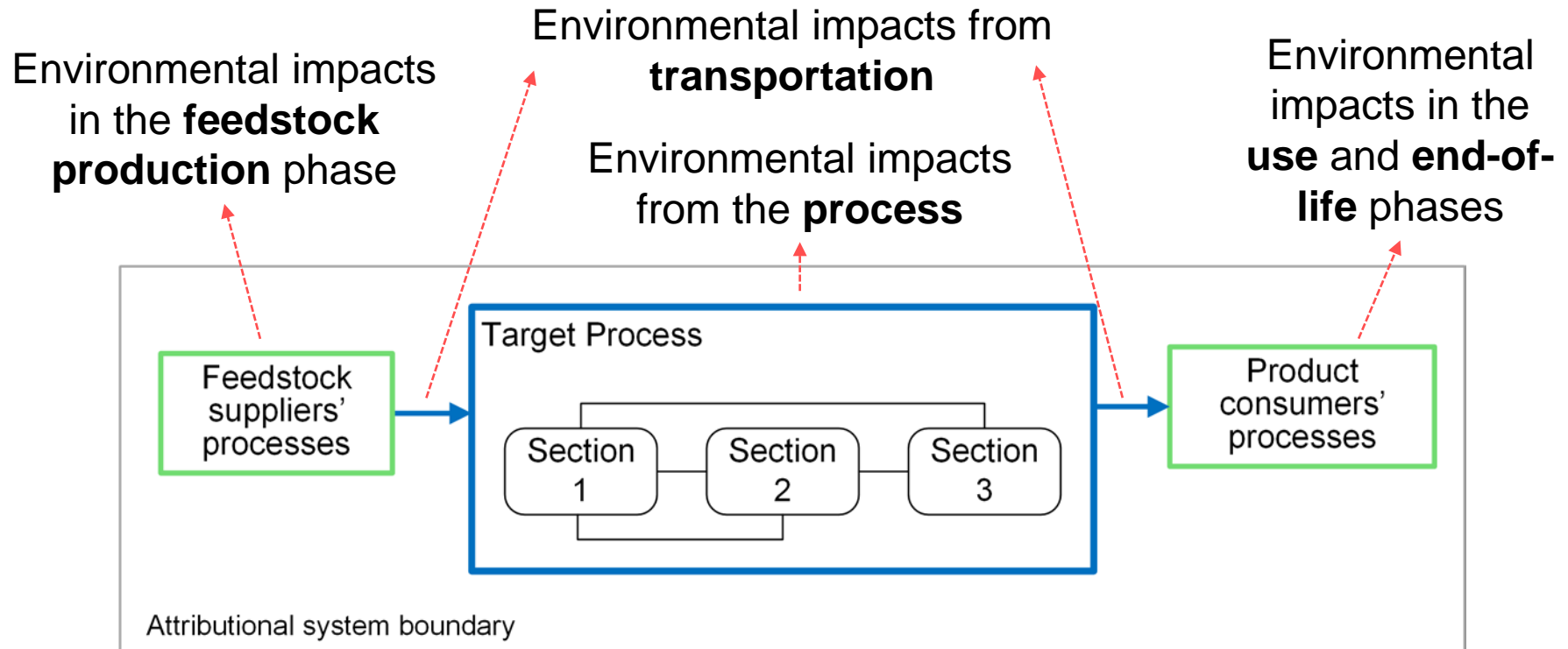
Before



After



Attributional LCA for Process Design Problems

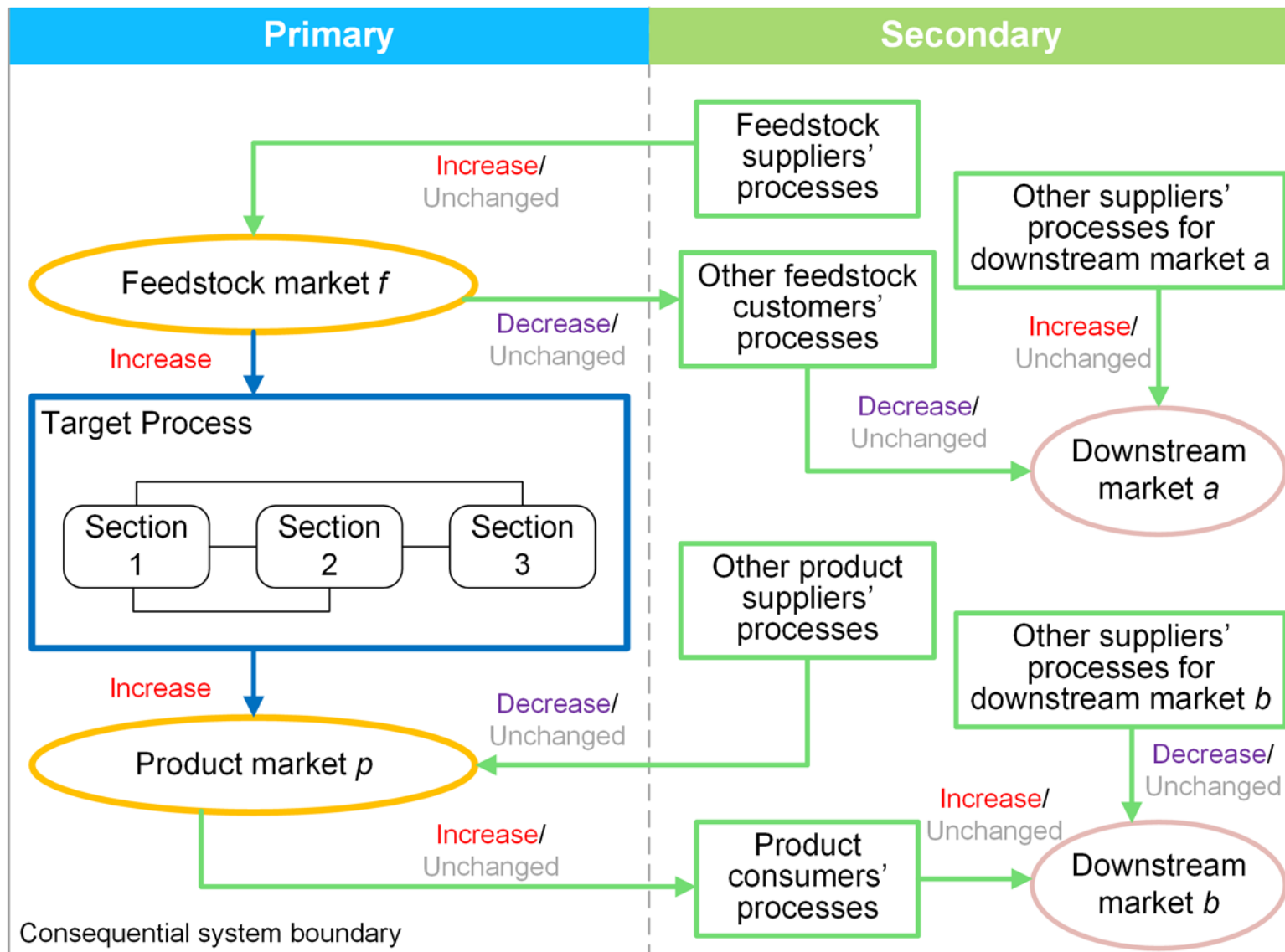


- Applicable to existing systems



- Not suitable for new systems
- Overlook the power of markets and influences in other processes

System Boundary of the Consequential LCO



Partial Equilibrium Model

Supply

$$as0_l = ad0_l, \quad \forall l$$

Demand

Aggregate supply function

$$AS_l = \sum_{p \in PPC_l} (asc_{l,p} \cdot XS_{l,p} + bsc_{l,p} \cdot YS_{l,p}) + PS_l, \quad \forall l$$

$$asc_{l,p} = \frac{ns_{l,p} - ns_{l,p-1}}{ms_{l,p} - ms_{l,p-1}}, \quad \forall l, p$$

$$bsc_{l,p} = ns_{l,p} - asc_{l,p} \cdot ms_{l,p}, \quad \forall l, p$$

$$\sum_{p \in PPC_l} YS_{l,p} = 1, \quad \forall l$$

$$\sum_{p \in PPC_l} XS_{l,p} = PR_l, \quad \forall l$$

$$ms_{l,p} \cdot YS_{l,p-1} \leq XS_{l,p} \leq ms_{l,p} \cdot YS_{l,p}, \quad \forall l, p$$

Price elasticity of demand

$$AD_l = \frac{ed_l \cdot \alpha_l}{\beta_l} \cdot PR_l + \alpha_l \cdot (1 - ed_l) + PD_l, \quad \forall l$$

Quantities by the target process

Equilibrium

$$AS_l = AD_l, \quad \forall l$$

$$LCI_l^{Supplier} = (AS_l - PS_l) - as0_l, \quad \forall l$$

$$LCI_l^{Customer} = (AD_l - PD_l) - ad0_l, \quad \forall l$$

Life Cycle Inventory

Consequential LCO framework

$$\max \sum_{k,l} h_{k,l} (P_l, Q_l, X_k, YC_k)$$

Economic Objective

e.g. maximize net present value

$$\min \sum_{l,r,s} [c_{l,r,s} \cdot v_{l,r,s} (Q_l, AS_l, AD_l)]$$

Environmental Objective

e.g. minimizing ReCiPe points

$$\text{s.t. } Q_l = \sum_k f_{k,l} (X_k, YP_k), \quad \forall l$$

Process Model

Integer variables for technology selection;
Mass and energy balance

$$AS_l = m_l (Q_l, P_l, YS_l), \quad \forall l$$

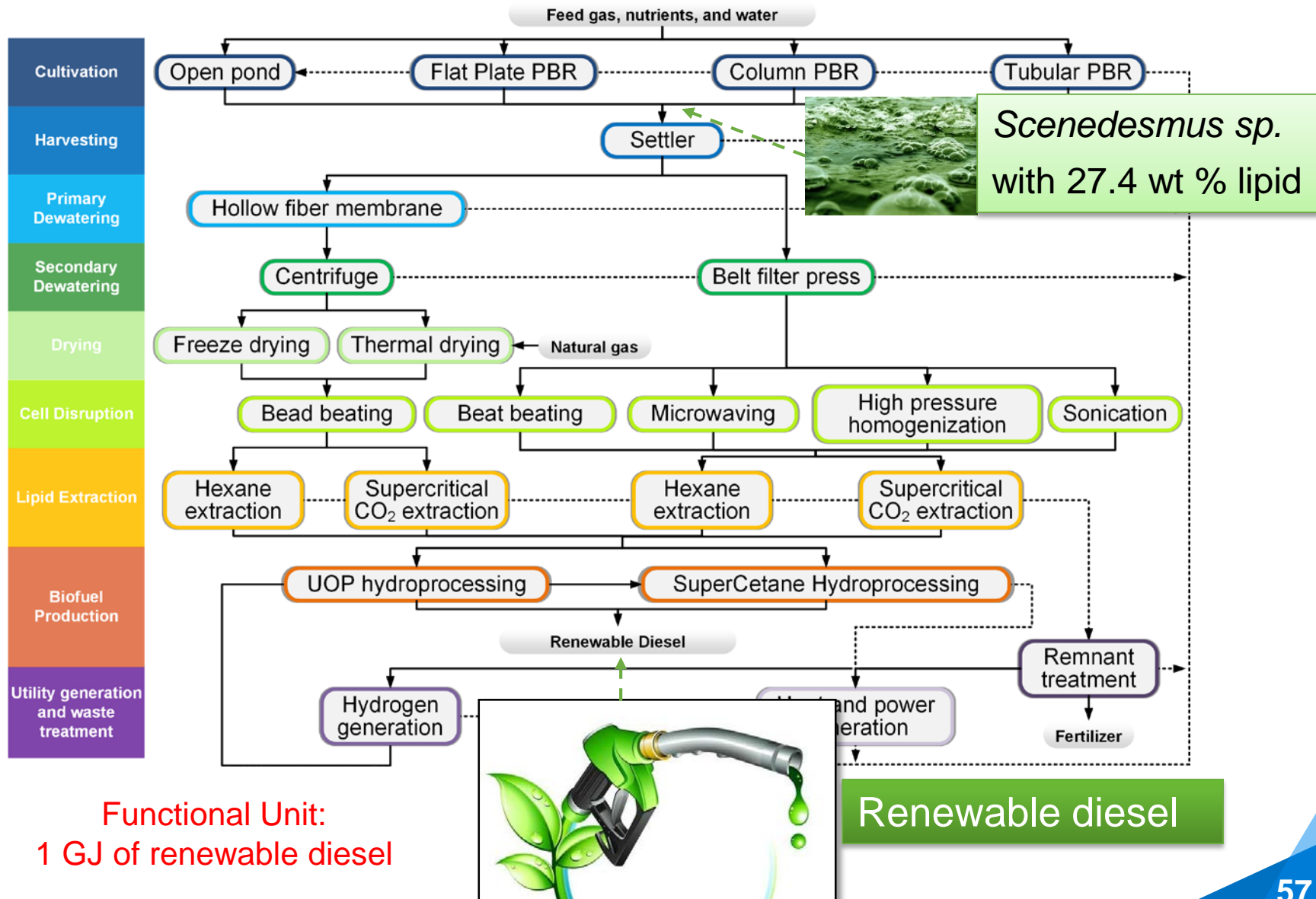
$$AD_l = n_l (Q_l, P_l, YD_l), \quad \forall l$$

$$AS_l = AD_l, \quad \forall l$$

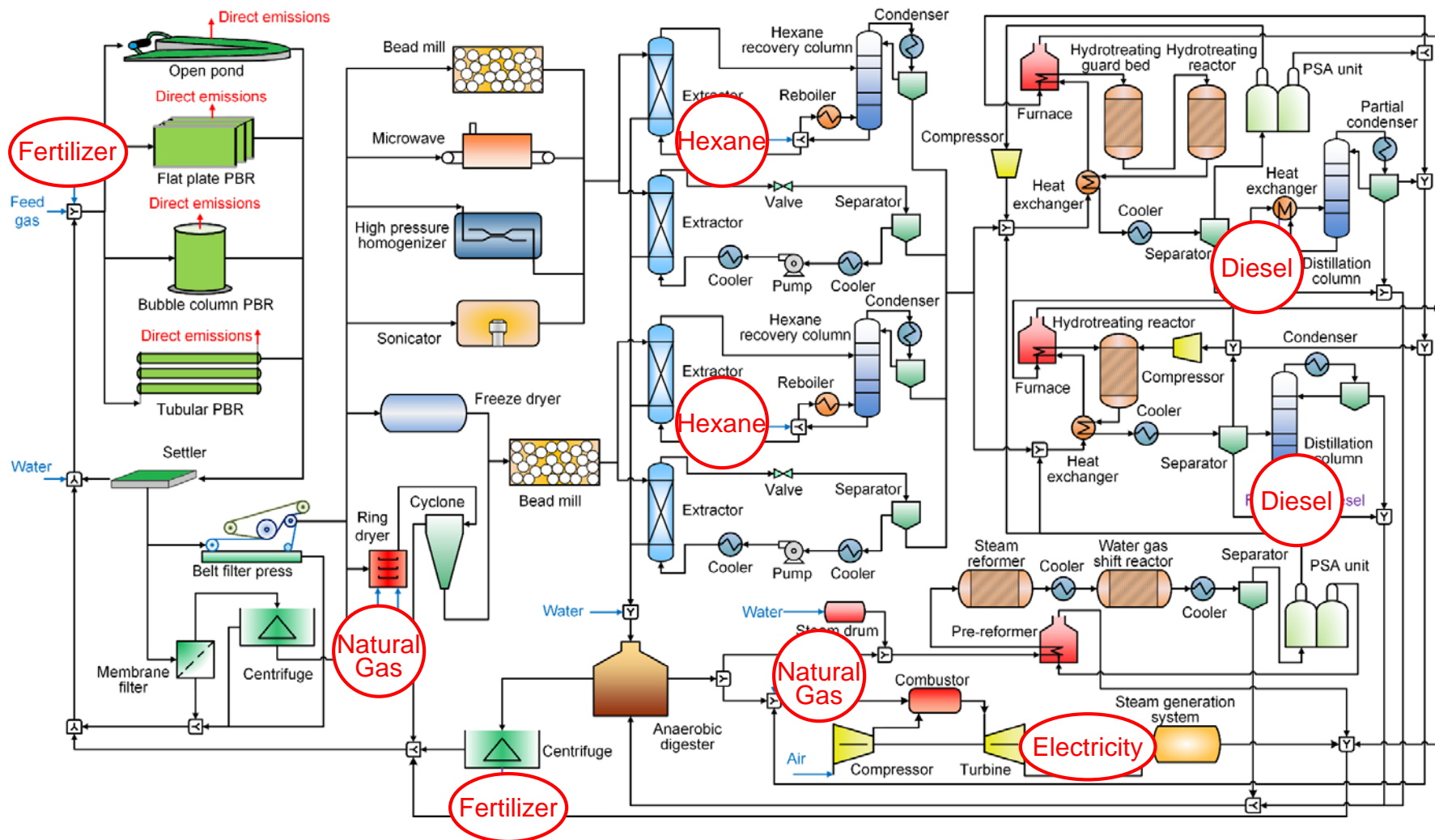
Market Model

Partial equilibrium models

Application to Algae-based Biofuel Production

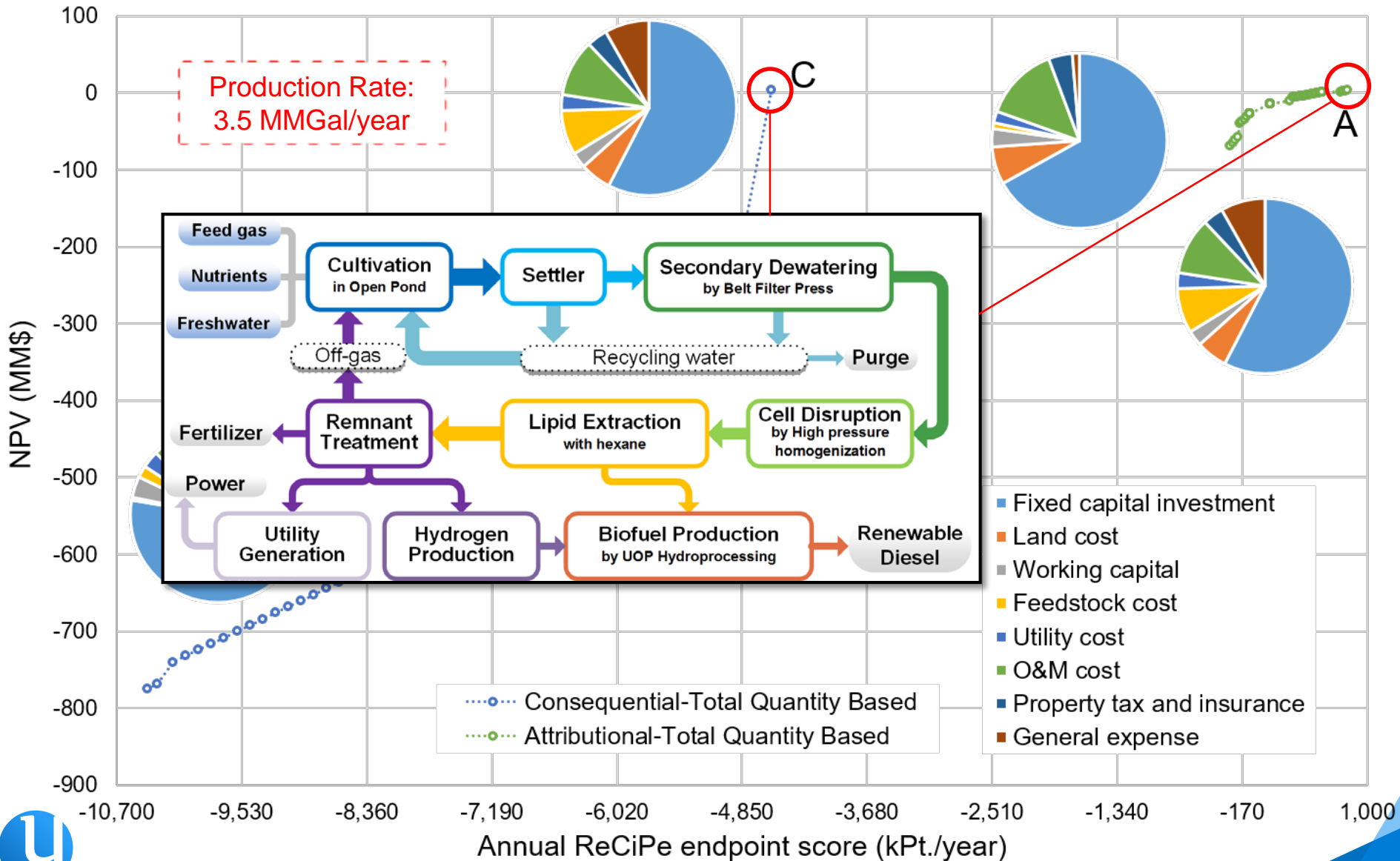


Detailed superstructure

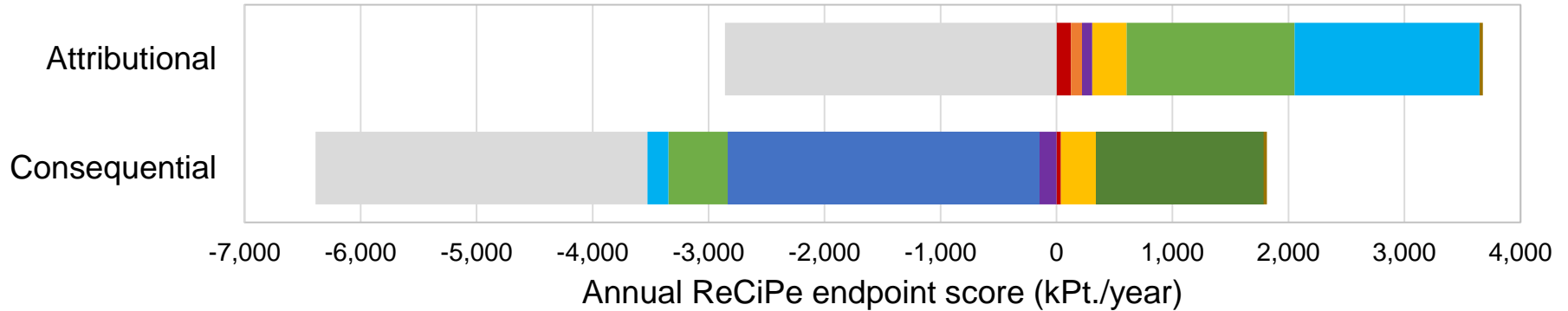


6 markets in the U.S.

Optimization Results for ReCiPe



Environmental Impact Breakdown

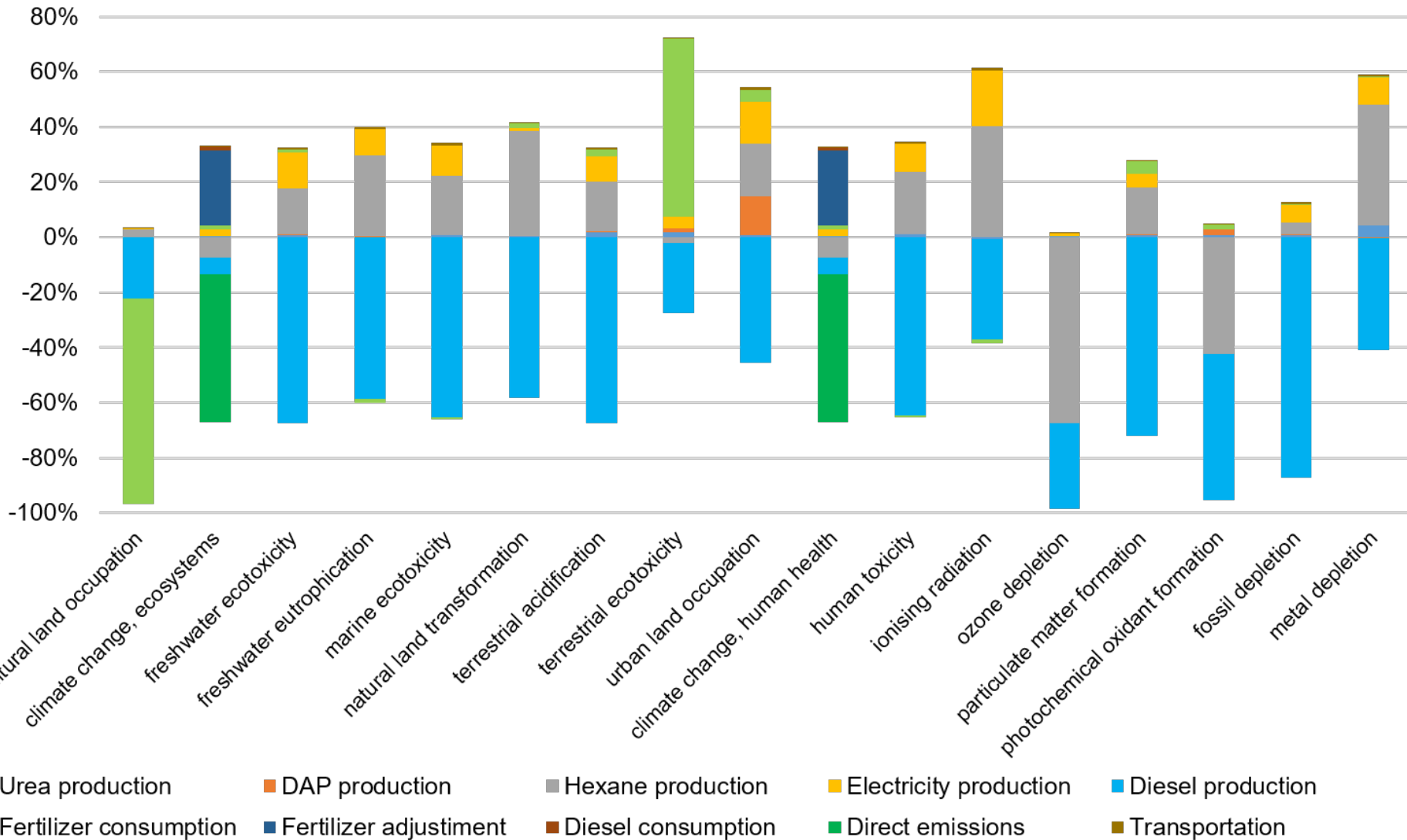


- Urea production
- Diesel production
- Direct emissions
- DAP production
- Fertilizer consumption
- Transportation
- Hexane production
- Fertilizer adjustment
- Electricity production
- Diesel consumption

Primary Markets	Attributional	Consequential
Fertilizers	Increase fertilizer production	(1) Increase but not as much; (2) Crops market (foreign ↑; domestic ↓)
Hexane	Positive characterization factors*	Negative characterization factors*
Diesel	Combustion in end of life	(1) Displace fossil diesel; (2) Transportation market (diesel ↑; gasoline ↓)

*Data for “rest of the world” from Ecoinvent 3.3

Consequential Environmental Profile



Consequential Life Cycle Optimization: General Conceptual Framework and Application to Algal Renewable Diesel Production

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Robert Frederick Smith School of Chemical and Biomolecular Engineering, Cornell University, 318 Olin Hall, Ithaca, New York 14853, United States

Supporting Information

ABSTRACT: Life cycle optimization (LCO) enables static life cycle analysis (LCA) and techno-economic analysis to be performed dynamically for automatic generation and optimization of process alternatives. Existing LCO models are developed following an attributional LCA approach, which overlooks the environmental consequences in response to the changes in the market. In this study, we develop a consequential LCO framework that simultaneously optimizes consequential environmental impacts and economic performance. We propose a general system boundary that encloses processes linked by markets. On the basis of the general system boundary, we develop a multiobjective optimization model, which integrates process models and market models

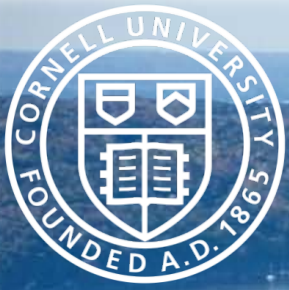
with the tenets of consequential LCA and techno-economic analysis methodologies. To efficiently solve the resulting nonconvex mixed-integer nonlinear programming problem, a global optimization algorithm is proposed to integrate the inexact parametric algorithm and the branch-and-refine algorithm. The application of the proposed framework is illustrated through a case study of producing renewable diesel from microalgae. We conduct detailed market analysis to identify the consequences associated with the renewable diesel production process. The environmental impacts of the optimal process designs based on the proposed consequential LCO framework are significantly lower than those based on the existing attributional LCO framework.

KEYWORDS: Life cycle optimization, Consequential life cycle analysis, Superstructure optimization, Sustainability, Algal biofuel



Conclusion

- **Life cycle analysis and life cycle optimization**
 - Process-level LCA and life cycle design/optimization
 - Systems boundary
 - Functional unit
 - **Integrated hybrid** LCA and LCO
 - Process systems to supply chain, and to macroeconomics scales
 - **Consequential** LCA and LCO
 - Dynamic and change-driven
 - Suitable for new product systems to account for influences of other processes through the market
- **Applications to energy systems**
 - Algal biorefinery
 - Shale gas
 -



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**Thank you for your attention
Questions?**