

# On-line Analysis – A Water Company Perspective

Peter Boruszenko – R&D Engineer

John Haley – Water Quality Compliance Manager

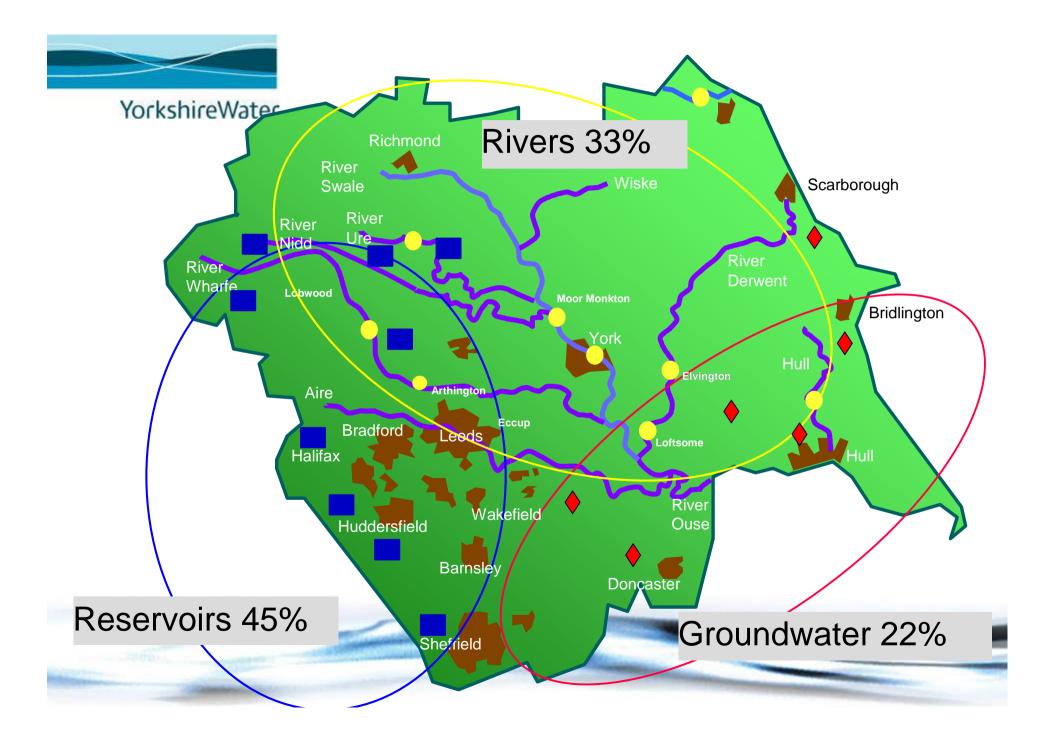
K. Clive Thompson ALcontrol Laboratories



## Introduction

- Why is on-line monitoring important to YW?
- 3 Case studies Online Monitoring for:-
  - Raw Water
  - Water Treatment
  - Distribution







## Why on-line analysis?

- Raw waters are variable
- Water treatment is rarely steady-state
- Best possible knowledge of risks to water quality
- Optimise treatment
- Manage risky situations
- Improved customer service







CASE STUDY 1: RAW WATER MONITORING

YorkshireWater

• There are over 15 million known organic substances.

•Robust technique to detect all of these? *Impossible !* 

- Compromise, pragmatism robustness, costs are key
- Not much TLC available OPEX limited!

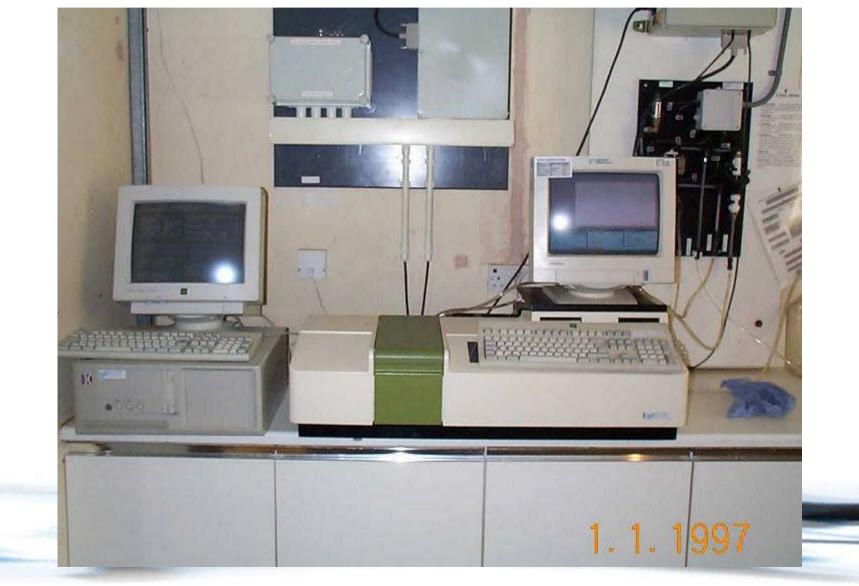




## On-line systems for river intake protection (11 sites) in YWS – position in 1986

- The Worcester & Dee Incidents made intake protection high profile
- Avoid supplying Water unfit for human consumption
  Due diligence defence
- Some companies have opted for highly intensive on-line analysis often specifically directed on the more potentially polluted rivers
- YW has relatively unpolluted rivers more widespread use of 'broad- band' monitors because we do not have known fixed contaminant risk!
- UV absorption detects a wide range of chemicals but not very sensitive in 1986 essentially detecting gross contamination.
- YW therefore developed the UV based system from first principles



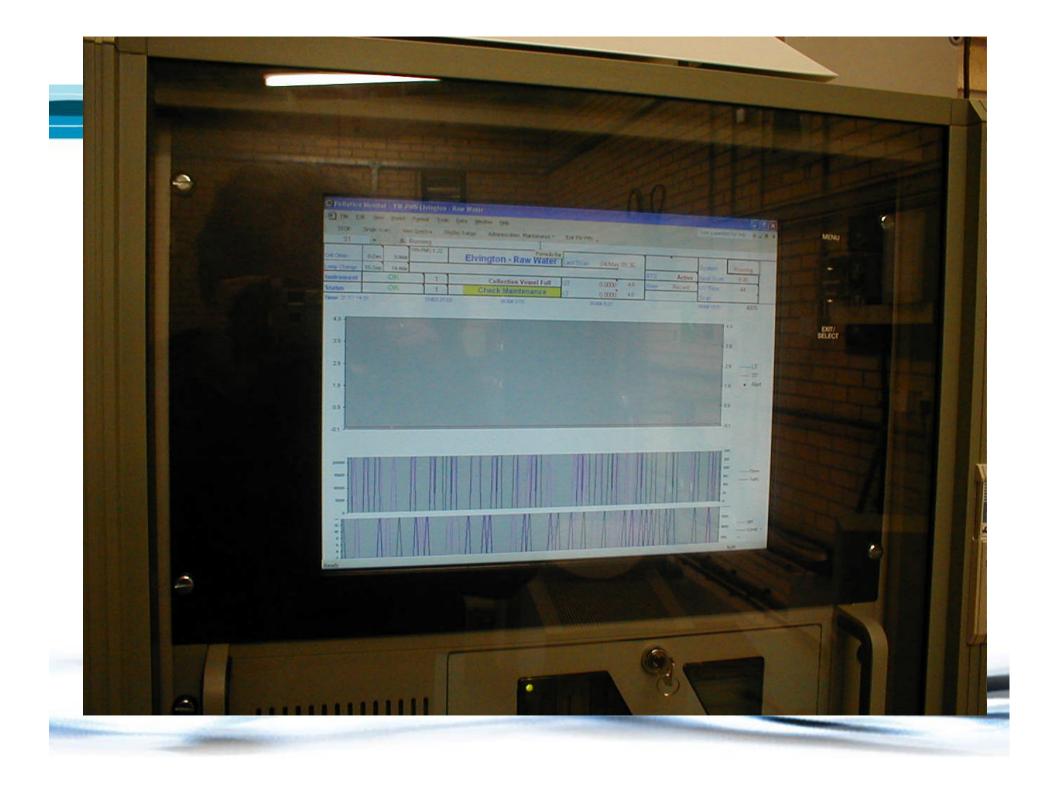


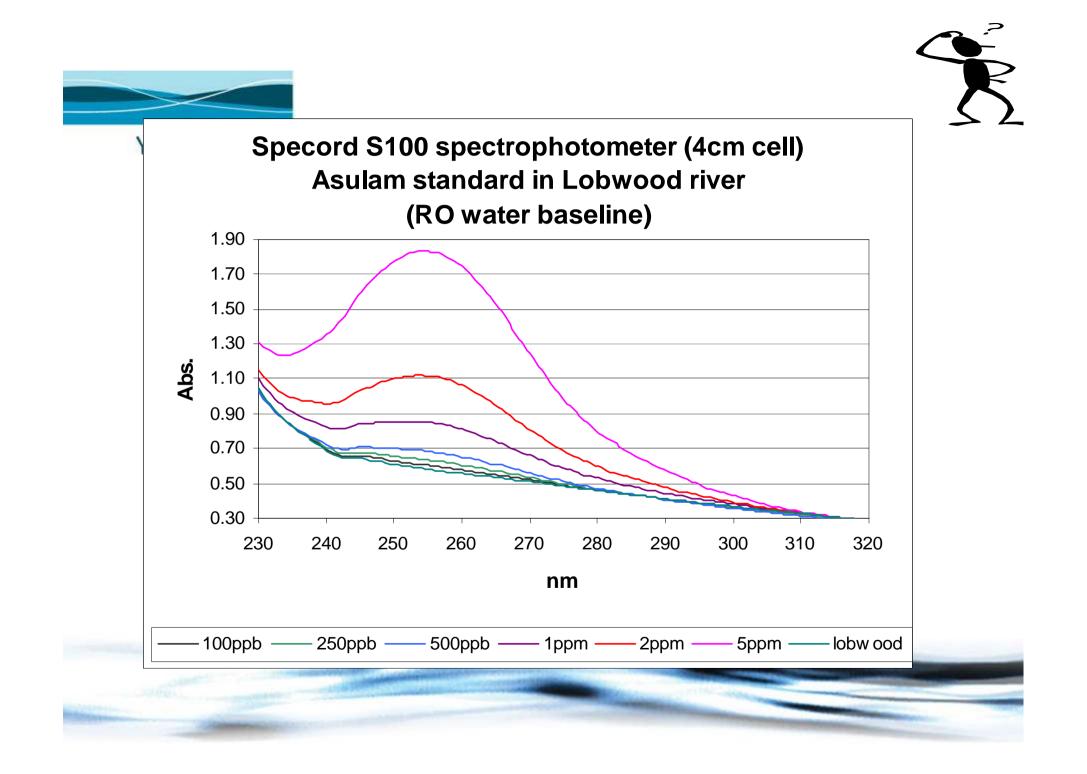


YorkshireWater On-line systems for river intake protection (11 sites) in YWS – position in 2002

- Decision made to re-examine systems for on-line monitoring from first principles
- Options considered and conclusion that broad screen monitoring most appropriate for YW rivers due to no specific risks.
- Some very expensive options on the market but no UV systems
- Decided that UV detection was the best process and to persuade a commercial supplier to develop a UV system with modern hardware and software









**On-line Monitors** 

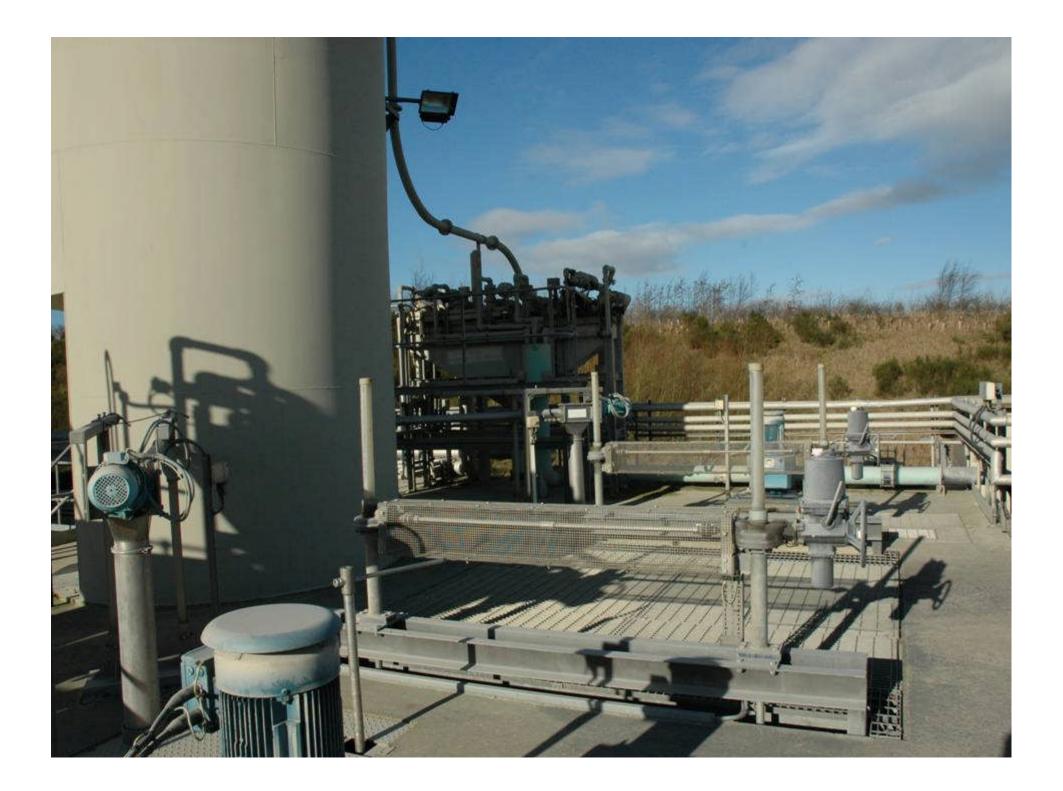
Key criteria

- Robust
- Low false positives
- Very low false negatives
- Sample pre-treatment for raw waters is key (*This is the 'Achilles heel' of many commercial systems*)
- Minimum preventative maintenance frequency: 1 visit / Month KEY ISSUE
- If there's no aromatic ring then it will not work.

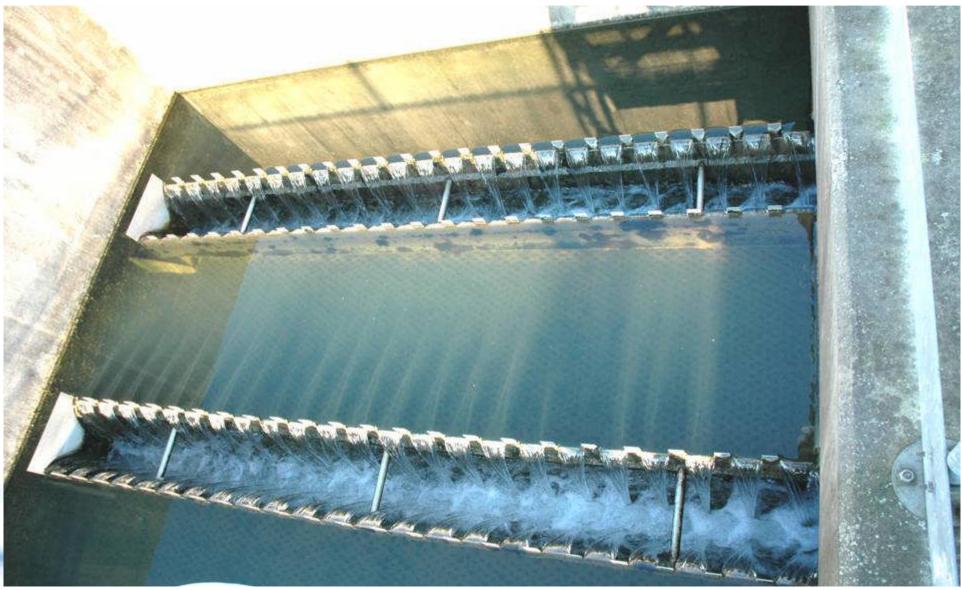


## CASE STUDY2: WATER TREATMENT Coagulation optimisation using on-line instrumentation





















## **Coagulation in Brief**

- Coagulant metal hydroxide precipitates to give floc.
- Coagulant only does this efficiently in a narrow pH band
- Colour particles stick to the **precipitating** coagulant hydrolysis products in the flash mixer (takes seconds)
- If there is not enough coagulant the colour particles give the precipitate a negative charge
  - Compromises optimum flocculation (small particles)
  - Compromises optimum filtration because charged particles won't stick to filter media at any time during the filter run.
- Overdosing of coagulant wastes money
  - Increases coagulant costs
  - Increases sludge production

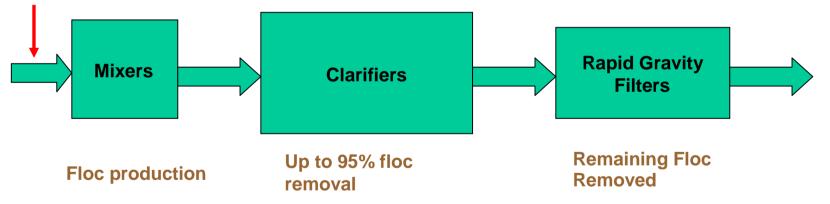




## Simplified Treatment Process

#### Add

- Aluminium or Ferric Sulphate (coagulant)
- Lime or Acid to control the pH of the mixture



#### **Products**





Turbidity

Observed relationships between filter outlet turbidity trend and degree of coagulation optimisation

#### YorkshireWater

BACKWASH

BASELINE

SPIKE

#### **Backwash Spike**

Wider and higher spike indicates lesser degree of coagulation optimisation.

#### **Baseline**

This distance is an indicator of coagulation optimisation.

Changing the coagulant dose (for a given raw water quality) changes this value.

Changing from optimum coagulation pH range to a different coagulation pH increases this value.

#### **Breakthrough**

Onset of break-through caused by **overloading filter** with small weak floc. Usually occurs in **winter/spring** at flotation sites.

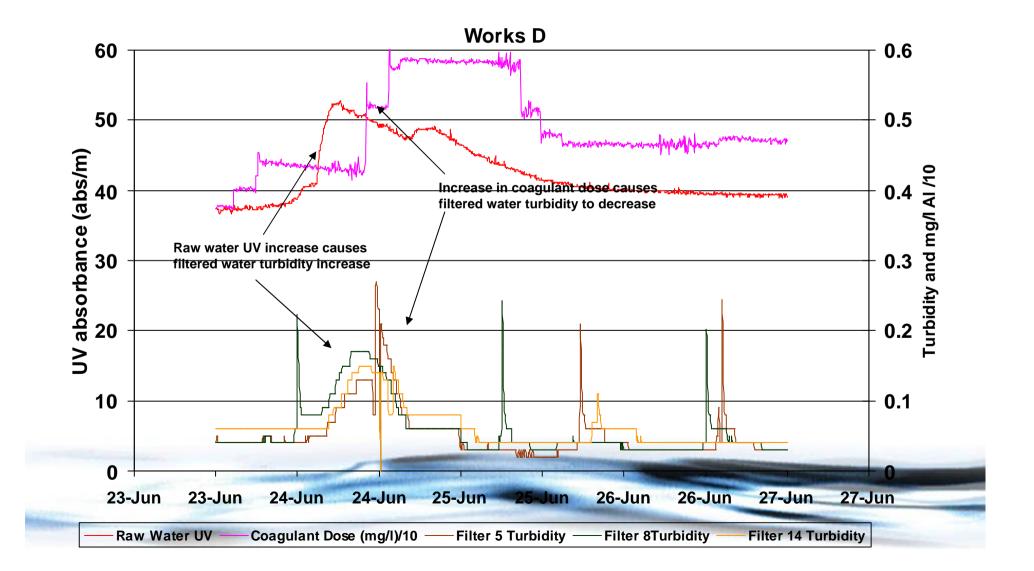
Made worse by increasing filtered water flow, increasing pre-filt turbidity and by flow surges through the filter.

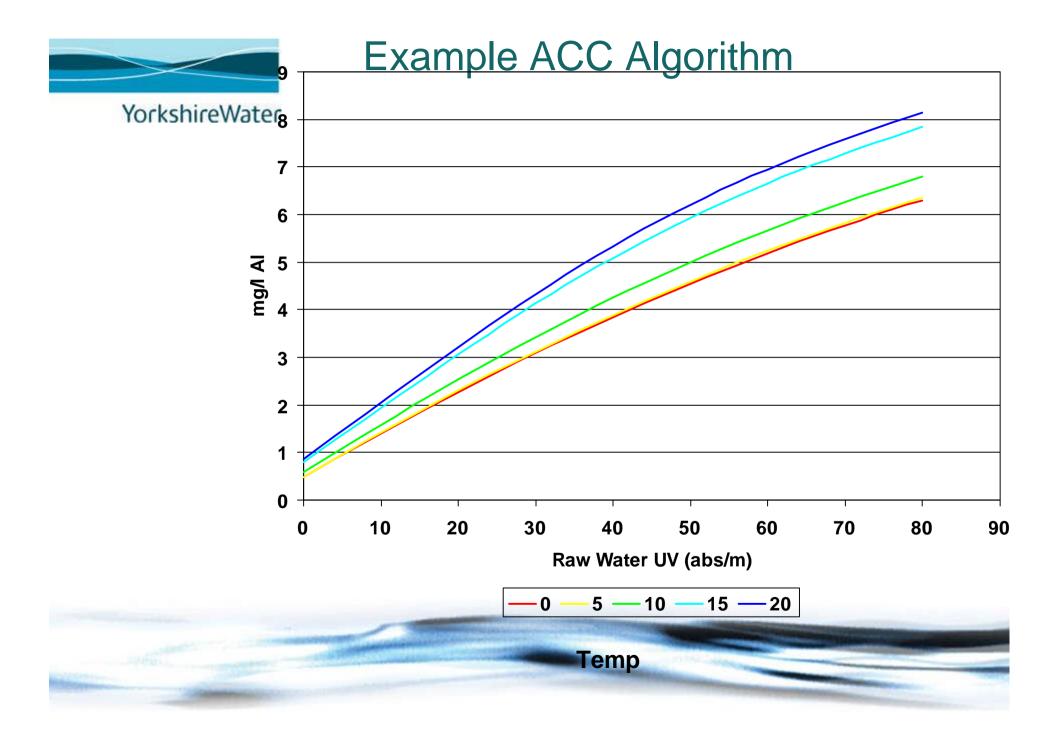
#### BREAKTHROUGH

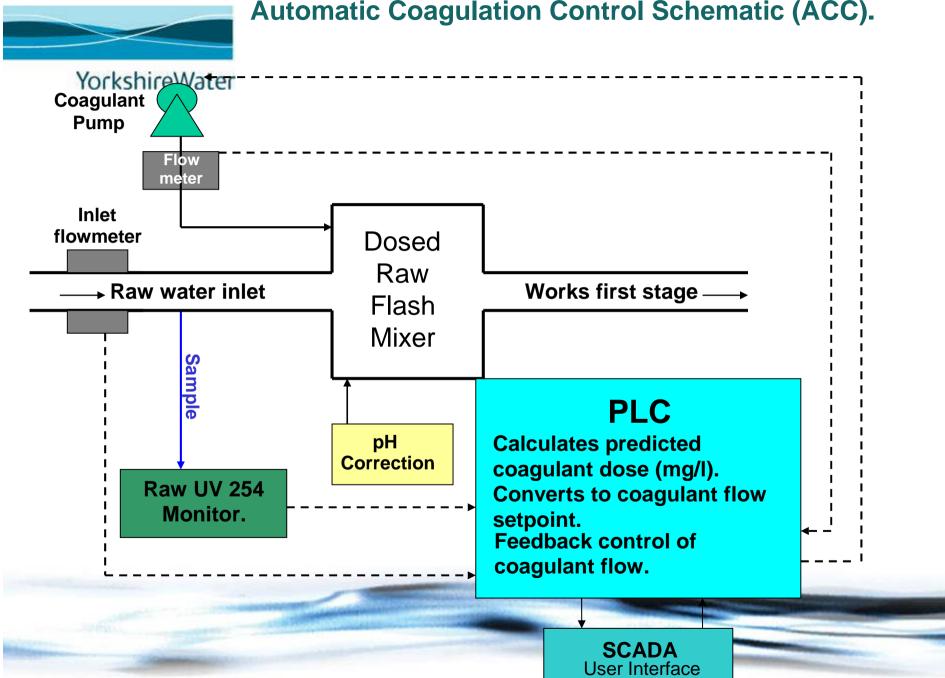
Time



## Raw water colour coagulant dose and filtered turbidity







#### Automatic Coagulation Control Schematic (ACC).









#### LONGWOOD WTW:

#### AUTO COAG CONTROL

#### COMMS STATUS E TELEMETRY INHIBITS 0 12/04/2006 14:18:21

E AC	5 K	
	COAGULATION CONTROL PRESETS	S
RAW WATER		-
Tu i	Adjustable dosing constant (K)	-2
- 0.0		0
	Dosing Lo Alarm (Underdose)	0
AW WATER	Predicted Dose Rate Hi Limit	0
pH	Tredicted Dose Nate Lo Linit	0
Pu	Actual Dose Rate Hi Limit	0
Bradsh	aw Actual Dose Rate Lo Limit	0
RAWWATER	2 C COAGULATION CONTROL PARAMETE	RS
	Turbidity Compensated Raw Water U	JV
	Raw Water Flow	
ABB 7320 R W 30.11	abs/m Supernatant Return Flow	_
DISSOLVED	Raw Water Colour Correction Factor	_
an a mulaa		
DRGANICS		Fa
DRGANICS	Raw Water Temperature Correction	Fa
ORGANICS	Raw Water Temperature Correction Predicted Ferric Dose (mg/l Fe)	_
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Maintenance Mode	Raw Water Temperature Correction Predicted Ferric Dose (mg/l Fe) Predicted Ferric Dose Rate (mg/l liqu Ferric Liquor Flow Setpoint	uor
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Set	Raw Water Temperature Correction Predicted Ferric Dose (mg/l Fe) Predicted Ferric Dose Rate (mg/l liqu Ferric Liquor Flow Setpoint Dosed Ferric Flow (Total from all purr Actual Ferric Dose Rate	nps

COAGULATION CONTROL PRESE Description	RANGE	PRES	NEW
Adjustable dosing constant (K)	-2.5 to 2.5	0.00	0.00
Dosing Hi Alarm (Overdose)	0 - 140 l/hr	45	45
Dosing Lo Alarm (Underdose)	0-70 l/hr	12	12
Predicted Dose Rate Hi Limit	0 - 17 mg/l Fe	11.0	11.0
Predicted Dose Rate Lo Limit	0-8 mg/l Fe	4.2	4.2
Actual Dose Rate Hi Limit	0 - 17 mg/IFe	11.0	11.0
Actual Dose Rate Lo Limit	0-8 mg/lFe	4.2	4.2

COAGULATION CONTROL PARAMETERS	CURRENT	UNITS
Turbidity Compensated Raw Water UV7320	30.11	abs/m
Raw Water Flow	21.57	TCMD
Supernatant Return Flow	-0.00	TCMD
Raw Water Colour Correction Factor	1.95	
Raw Water Temperature Correction Factor	0.02	
Predicted Ferric Dose (mg/l Fe)	5.69	mg/IFe
Predicted Ferric Dose Rate (mg/l liquor)	42.15	mg/l liquor
Ferric Liquor Flow Setpoint	23.66	I/hr
Dosed Ferric Flow (Total from all pumps)	23.30	l/hr



<u>></u>

OK

OK

ACC SYSTEM STATUS	OK
ACC MODE	ACC
UV7320 SAMPLE FLOW	OK
UV7320 RATE OF CHANGE	OK
SETPOINT NOT ACHIEVED	OK

Launch complete Refresh FERRIC DOSING ACC RESET ≜ 🕸 📩 👬 🚟 🕺 🐼 ? A 🕄 💷 PRE 2ND STAGE CL2 OUT OF RANGE

LOSS OF HEAD FILTER2 OUT OF RANGE

14:00:55.000 CA6\_QT2000OR 13:21:01.100 CA9 T32500OR

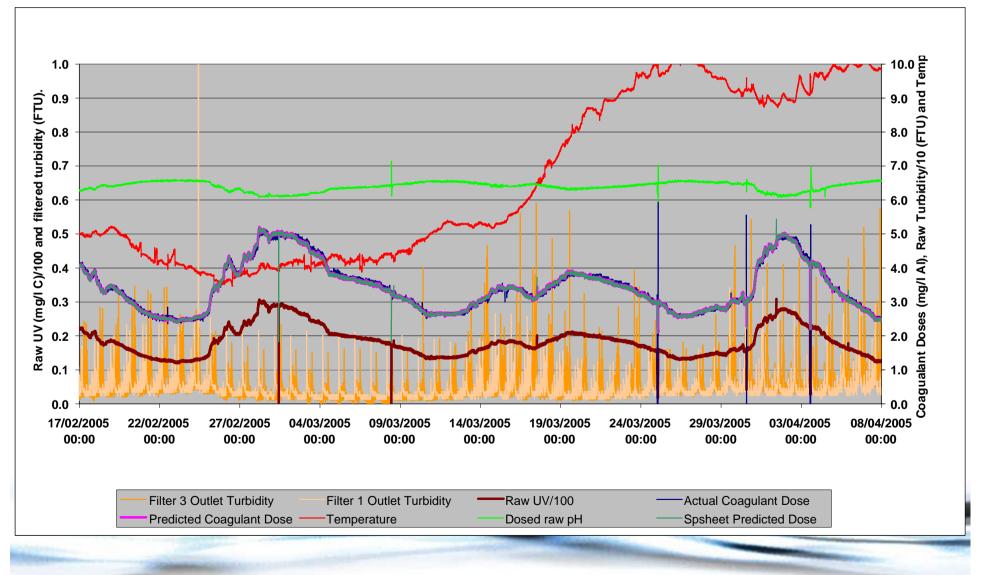
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#### ACC Example – River Works (Site F)





## **Conclusions**

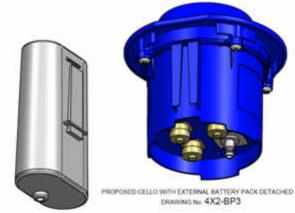
The ACC System:-

- Reduces the need for manual intervention
- Reduces overdosing of Coagulant
  - (1500 Tonnes in 11 months)
- Reduces out-of-hours call-outs
- Maintains optimum treated water turbidity
- Minimises risk of Cryptosporidium breakthrough

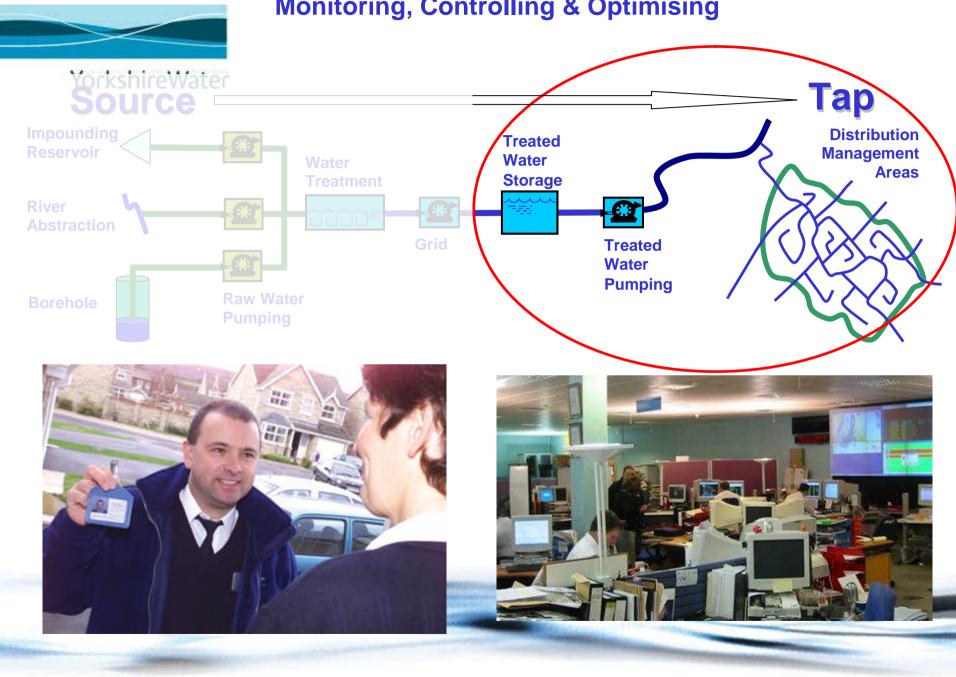


## **CASE STUDY 3 - DISTRIBUTION**

# Real Time Network







#### Monitoring, Controlling & Optimising



## **RTnet Drivers**

- 1. Reduce/Remove manual data collection
- 2. Leakage data on a daily basis
- 3. Receive customer service data every half hour

### 'Respond to failure before the customer is impacted'





## Key Issues

- Communications
- Battery life
  - Currently only 2.5 years
  - Power harvesting?
- Managing the data
- COST !!!





## **Future Issues**

- Rtnet only measure at zone inlets...
  How do we measure rest of the network
- Measure real time water quality:
  - In distribution
  - At service reservoirs
- Multi-functioning device
  - Water quality, pressure, flow
  - CENSAR





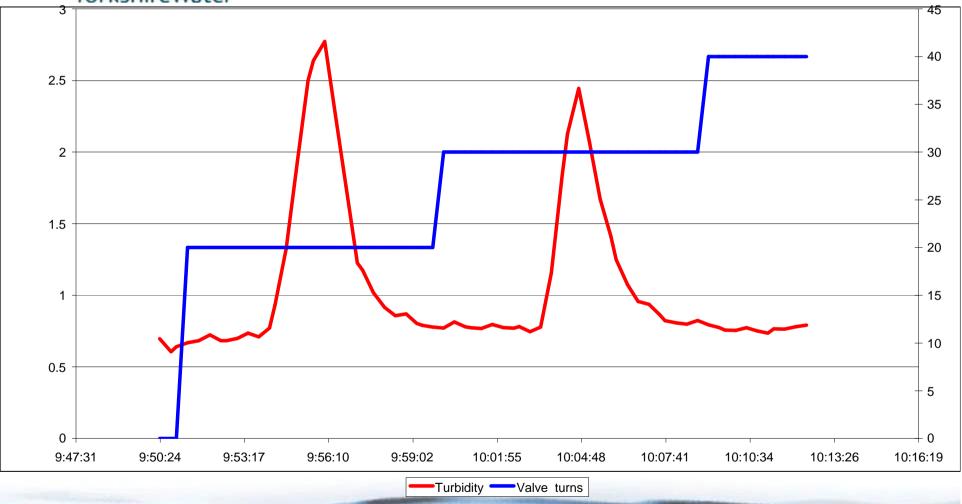


This is very heavy – a two man operation – also attenuates signals





## Initial Closure Turbidity Effects





## CONCLUSIONS

YorkshireWater

- There is a widespread move away from manual intervention in water treatment process control
- 20 new sites require robust reliable pollution monitors various new systems are being considered.
- At least one month unattended operation is essential
- Enhanced customer service

Attain top position in the OEWAT league table !



## **Discussion / Questions**

